

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
4 April 2002 (04.04.2002)

PCT

(10) International Publication Number
WO 02/26836 A2

(51) International Patent Classification⁷: C08F 2/38,
293/00, C07C 337/08

(74) Agent: KRASNOW, Ronald, A.; Symyx Technologies,
Inc., 3100 Central Expressway, Santa Clara, CA 95051
(US).

(21) International Application Number: PCT/US01/30066

(81) Designated States (national): AE, AG, AL, AM, AT, AU,
AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU,
CZ, DE, DK, DM, DZ, EC, EG, ES, FI, GB, GD, GE, GH,
GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC,
LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW,
MX, MZ, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK,
SL, TJ, TM, TR, TT, TZ, UA, UG, UZ, VN, YU, ZA, ZW.

(22) International Filing Date:
26 September 2001 (26.09.2001)

(25) Filing Language: English

(84) Designated States (regional): ARIPO patent (GH, GM,
KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW), Eurasian
patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European
patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE,
IT, LU, MC, NL, PT, SE, TR), OAPI patent (BF, BJ, CF,
CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD,
TG).

(26) Publication Language: English

(30) Priority Data:
09/676,267 28 September 2000 (28.09.2000) US
09/963,172 25 September 2001 (25.09.2001) US

(71) Applicant: SYMYX TECHNOLOGIES, INC. [—/US];
3100 Central Expressway, Santa Clara, CA 95051 (US).

Published:

— without international search report and to be republished
upon receipt of that report

For two-letter codes and other abbreviations, refer to the "Guid-
ance Notes on Codes and Abbreviations" appearing at the begin-
ning of each regular issue of the PCT Gazette.

(72) Inventors: CHARMOT, Dominique; 1238 Bracebridge
Court, Campbell, CA 95008 (US). CHANG, Han, Ting;
220 Garnet Drive, Livermore, CA 94550 (US). LI, Yunx-
iao; 737E. El Camino Real, Sunnyvale, CA 94087 (US).
HUEFNER, Peter; 634 Celebration Court, San Jose, CA
95134 (US).

WO 02/26836 A2

(54) Title: CONTROL AGENTS FOR LIVING-TYPE FREE RADICAL POLYMERIZATION, METHODS OF POLYMERIZ-
ING, EMULSIONS AND POLYMERS WITH SAME

(57) Abstract: Control agents that have a nitrogen-nitrogen bond covalently bonded to a thiocarbonyl moiety are provided for living-type free radical polymerization of a wide variety of monomers. These control agents provide superior properties for control of the polymerization and/or the properties of the polymers obtained and/or the monomers that may be polymerized. In some embodiments, a bulky group is pendant off the activated thiocarbonyl portion of the control agents. Multifunctional control agents provide the opportunity for a variety of structurally unique polymers, including block copolymers, stars and hyper-branched polymers.

5 CONTROL AGENTS FOR LIVING-TYPE FREE RADICAL POLYMERIZATION, METHODS OF POLYMERIZING, EMULSIONS AND POLYMERS WITH SAME

FIELD OF THE INVENTION

10

[0001] The present invention relates to new compounds useful in assisting in the polymerization of monomers in a free radical polymerization that has living-type kinetics. Polymers made with the control agents and processes for polymerization are also included. In addition, some of the compounds themselves are novel.

15

BACKGROUND OF THE INVENTION

[0002] The use and mechanism of control agents for free radical polymerization is now generally known, see for example U.S. Patent No. 6,153,705, WO98/01478, 20 WO99/35177, WO99/31144, and WO98/58974, each of which is incorporated herein by reference. Despite this knowledge, no successful commercialization of a polymerization process has occurred with these agents. Thus the need for new agents, which lead to a commercializable process are needed.

[0003] In addition, the previously known control agents have limited uses. Although 25 touted as universally useful, those of skill in the art appreciate that a particular control agent is particularly useful for the control of particular monomers and monomer mixtures. The polymerization conditions under which particular control agents are particularly useful are generally not well known. Thus, a need exists for a family of related control agents that can be easily synthesized and modified so that a control agent 30 will be readily available for polymerizing desired monomers under commercially acceptable conditions, which include high conversion at the shortest possible reaction times and lower temperatures

[0004] Additionally, there is a strong need in the industry to make block copolymers in emulsion processes. From a process point of view, emulsions are advantageous over 35 bulk or solution processes because emulsion processes allow for relative ease of heat

removal, use of environmentally friendly water as liquid vehicle (as compared to organic solvents), ease of polymer handling and purification (e.g., stripping off residual monomers), high solid content with high molecular weight, and relatively low cost operations. From an application point of view, emulsion polymers currently are used 5 extensively in waterborne formulations (such as coating, adhesives, and textiles). The preparation of block copolymers in an emulsion has long been sought for without commercializable results. Although resin emulsification techniques have been used to form emulsions of thermoplastic elastomers (such as polystyrene-b-polydiene-b-polystyrene triblock copolymers), there has been no commercial significance due to high 10 costs and limited chemical composition ranges.

[0005] Recently, living free radical polymerization (LFRP) (sometimes referred to as controlled free radical polymerization) has been shown to be a viable technique to 15 prepare a large diversity of block copolymers. However, despite many attempts, none of these techniques have currently lead to commercial processes when applied in emulsion polymerization. Nitroxide mediated LFRP can require temperatures inappropriate for emulsion processes, with nitroxide mini-emulsion processes providing acceptable results, but with drastically limited industrial applicability. ATRP has the main drawback of 20 introducing heavy metals in the final emulsion, which causes environmental concerns and also is detrimental to the latex stability. Several reports have shown that dithioesters in RAFT emulsion polymerization produce substantial retardation, latex that contains high level of grit, and polymer with poor control (e.g., polydispersity of 1.8 and higher) (see, for example, *Journal of Polymer Science: Part A : Polymer Chemistry*, Vol. 38, 25 3864-3874, 2000). Mini-emulsions have been used to alleviate these difficulties to some extent, but again this very much limits its industrial application. Moreover dithioesters impart a deep pink color to the final emulsions. Other dithioccompounds, such as 30 dithiocarbonates (xanthates) are less prone to grit formation, but they exhibit much less control over polymer characteristics, such as polydispersity than dithioesters, dithiocarbarnates and dithiocarbazates. For instance polydispersity of 3 are reported for the emulsion polymerization of butyl acrylate and styrene when dithiocarbonates are used, see. e.g., *Macromolecular Symposia*, 2000, 150, 23 and *Journal of Polymer Science: Part A: Polymer Chemistry*, Vol. 38, 4206-4217, 2000.

[0006] This invention solves these issues by providing control agents that can be easily modified for particular monomers and monomer mixtures in emulsion systems. Certain

dithiocarbazates have superior properties in providing good control over the polymer characteristics together with good latex stability and a high rate of polymerization.

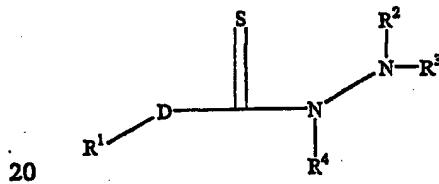
[0007] This invention provides control agents that can be easily modified for particular monomers and monomer mixtures. The control agents of the present invention contain at least one nitrogen—nitrogen bond, which allows for simpler modification of the electronic and steric nature of the control agents as compared to known control agents. These modified properties allow for improved conditions of the polymerization process and/or improved properties of the polymers obtained from the processes.

10

SUMMARY OF THE INVENTION

[0008] This invention provides control agents that are easy to prepare and economically useful on a commercial scale. In particular, the control agents of this invention have a nitrogen-nitrogen bond, which is believed to provide better chemical stability of the control agent together with a greater flexibility for chemical modification of said control agents, while giving control of a polymerization reaction that includes a free radical.

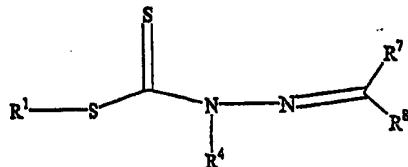
[0009] In general, the control agents of this invention have a N-N bond covalently bonded to a thiocarbonyl moiety. In some embodiments the control agents can be characterized by the general formula:



wherein D is S, Te or Se; R¹ is generally any group that is sufficiently labile to be expelled as its free radical form; R² and R³ are each independently selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof, and R⁴ is selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof; and optionally, R⁴ combines with R² to form a ring structure, with said ring having from 3 to 50 non-hydrogen atoms. In some embodiments, R² can form a ring structure with R¹, as discussed herein.

[0010] Another aspect of this invention is directed toward multi-functional control agents, so that the control agents may occupy either a central portion of a polymer chain and/or two or more ends of a polymer. In those embodiments where the control agent occupies a central portion of the polymer backbone, the nitrogen-nitrogen bond provides 5 the unique opportunity to degrade the polymer backbone into smaller pieces by external stimuli (e.g., heat, chemical reaction, irradiation, etc.). Such a process is unique as compared to known free radical polymerization and "living" free radical polymerization techniques. In addition, some of the multi-functional control agents are cyclic, which provide the unique opportunity to prepare block copolymers with reduced processes 10 steps. Furthermore, some multi-functional control agents allow for ring opening polymerizations, which heretofore have not found commercial applications in free radical polymerization.

[0011] In another aspect, this invention provides control agents that are easy to prepare and economically useful on a commercial scale in emulsion. In general, the control 15 agents of this embodiment have a N-N bond covalently bonded to a thiocarbonyl moiety, with an optionally substituted double bonded alkenyl moiety. The control agents can be characterized by the general formula:



wherein R¹ is generally any group that is sufficiently labile to be expelled as its free 20 radical form; R⁴ is selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof; and R⁷ and R⁸ are independently selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, 25 and combinations thereof. These control agents are used in an emulsion polymerization process by forming a heterogeneous mixture and subjecting that mixture to polymerization conditions. The heterogeneous mixture comprises the control agent, one or more monomers, water, initiator and optionally surfactant. Polymerization conditions include the pressure, temperature and other process conditions, such a polymerization 30 method (e.g., batch, semi-batch or continuous).

[0012] Other aspects of this invention include certain of the control agents, which are novel compounds. Polymerization processes using all of the control agents of this invention and polymers that can be made with the control agents of this invention are additional aspects of this invention. In particular, the control agents of this invention 5 provide living-type kinetics and as such allow for the preparation of desired products, including block polymers, star architectures, grafts and hyperbranched polymers.

[0013] Thus, it is an object of this invention to provide novel control agents for a living-type free radical polymerization process.

[0014] It is another object of this invention to provide novel compounds, which are 10 useful as control agents in a free radical polymerization process.

[0015] It is a further object of this invention to provide a novel system for free radical polymerization of monomers that employs living-type kinetics.

[0016] It is still a further object of this invention to polymerize a variety of monomers under commercially acceptable conditions with a family of control agents.

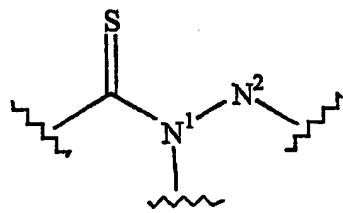
[0017] It is yet a further object of this invention to make controlled architecture 15 polymers with a polymerization process that employs a control agent.

[0018] It is further another object of this invention to provide multifunctional control agents that may occupy a central portion of a polymer chain allowing for the polymer chain to be degraded.

[0019] Further aspects and objects of this invention will be evident to those of skill in the 20 art upon review of this specification.

DETAILED DESCRIPTION OF THE INVENTION

[0020] In the most general terms, the control agents of this invention contain at least one 25 N^1-N^2 bond covalently bonded to a thiocarbonyl group. In structural terms, the following moiety must be present in the control agents of this invention:



In some embodiments, a sulfur atom is attached to the thiocarbonyl group, leading to a dithiocarbonyl moiety. This may be referred to herein as the "dithiocarbazate" group or

N-NC(=S)S moiety, however, such terminology is not intended to be limiting. Also, in some embodiments, the substituents of N² (other than N¹) should not form a heterocycle that includes N².

5 [0021] In describing and claiming the present invention, the following terminology will be used in accordance with the definitions set out below. A named R group will generally have the structure that is recognized in the art as corresponding to R groups having that name. For the purposes of illustration, representative R groups as

enumerated above are defined herein. These definitions are intended to supplement and illustrate, not preclude, the definitions known to those of skill in the art.

10 [0022] It is also to be understood that the terminology used herein is for the purpose of describing particular embodiments only, and is not intended to be limiting. As used in this specification and the appended claims, the singular forms "a," "an" and "the" include plural referents unless the context clearly dictates otherwise. In describing and claiming the present invention, the following terminology will be used in accordance 15 with the definitions set out below.

[0023] The following definitions pertain to chemical structures, molecular segments and substituents:

20 [0024] As used herein, the phrase "having the structure" is not intended to be limiting and is used in the same way that the term "comprising" is commonly used. The term "independently selected from the group consisting of" is used herein to indicate that the recited elements, e.g., R groups or the like, can be identical or different (e.g., R² and R³ in the structure of formula (1) may all be substituted alkyl groups, or R² may be hydrido and R³ may be methyl, etc.).

25 [0025] "Optional" or "optionally" means that the subsequently described event or circumstance may or may not occur, and that the description includes instances where said event or circumstance occurs and instances where it does not. For example, the phrase "optionally substituted hydrocarbyl" means that a hydrocarbyl moiety may or may not be substituted and that the description includes both unsubstituted hydrocarbyl and hydrocarbyl where there is substitution.

30 [0026] The term "alkyl" as used herein refers to a branched or unbranched saturated hydrocarbon group typically although not necessarily containing 1 to about 24 carbon atoms, such as methyl, ethyl, n-propyl, isopropyl, n-butyl, isobutyl, t-butyl, octyl, decyl, and the like, as well as cycloalkyl groups such as cyclopentyl, cyclohexyl and the like.

Generally, although again not necessarily, alkyl groups herein contain 1 to about 12 carbon atoms. The term "lower alkyl" intends an alkyl group of one to six carbon atoms, preferably one to four carbon atoms. "Substituted alkyl" refers to alkyl substituted with one or more substituent groups, and the terms "heteroatom-containing alkyl" and 5 "heteroalkyl" refer to alkyl in which at least one carbon atom is replaced with a heteroatom.

[0027] The term "alkenyl" as used herein refers to a branched or unbranched hydrocarbon group typically although not necessarily containing 2 to about 24 carbon atoms and at least one double bond, such as ethenyl, *n*-propenyl, isopropenyl, *n*-butenyl, 10 isobut enyl, octenyl, decenyl, and the like. Generally, although again not necessarily, alkenyl groups herein contain 2 to about 12 carbon atoms. The term "lower alkenyl" intends an alkenyl group of two to six carbon atoms, preferably two to four carbon atoms. "Substituted alkenyl" refers to alkenyl substituted with one or more substituent groups, and the terms "heteroatom-containing alkenyl" and "heteroalkenyl" refer to 15 alkenyl in which at least one carbon atom is replaced with a heteroatom.

[0028] The term "alkynyl" as used herein refers to a branched or unbranched hydrocarbon group typically although not necessarily containing 2 to about 24 carbon atoms and at least one triple bond, such as ethynyl, *n*-propynyl, isopropynyl, *n*-butynyl, isobutynyl, octynyl, decynyl, and the like. Generally, although again not necessarily, 20 alkynyl groups herein contain 2 to about 12 carbon atoms. The term "lower alkynyl" intends an alkynyl group of two to six carbon atoms, preferably three or four carbon atoms. "Substituted alkynyl" refers to alkynyl substituted with one or more substituent groups, and the terms "heteroatom-containing alkynyl" and "heteroalkynyl" refer to alkynyl in which at least one carbon atom is replaced with a heteroatom.

[0029] The term "alkoxy" as used herein intends an alkyl group bound through a single, terminal ether linkage; that is, an "alkoxy" group may be represented as -O-alkyl where alkyl is as defined above. A "lower alkoxy" group intends an alkoxy group containing one to six, more preferably one to four, carbon atoms. The term "aryloxy" is used in a similar fashion, with aryl as defined below.

[0030] Similarly, the term "alkyl thio" as used herein intends an alkyl group bound through a single, terminal thioether linkage; that is, an "alkyl thio" group may be represented as -S-alkyl where alkyl is as defined above. A "lower alkyl thio" group

intends an alkyl thio group containing one to six, more preferably one to four, carbon atoms.

[0031] The term "allenyl" is used herein in the conventional sense to refer to a molecular segment having the structure —CH=C=CH₂. An "allenyl" group may be unsubstituted or substituted with one or more non-hydrogen substituents.

[0032] The term "aryl" as used herein, and unless otherwise specified, refers to an aromatic substituent containing a single aromatic ring or multiple aromatic rings that are fused together, linked covalently, or linked to a common group such as a methylene or ethylene moiety. The common linking group may also be a carbonyl as in benzophenone, an oxygen atom as in diphenylether, or a nitrogen atom as in diphenylamine. Preferred aryl groups contain one aromatic ring or two fused or linked aromatic rings, e.g., phenyl, naphthyl, biphenyl, diphenylether, diphenylamine, benzophenone, and the like. In particular embodiments, aryl substituents have 1 to about 200 carbon atoms, typically 1 to about 50 carbon atoms, and preferably 1 to about 20 carbon atoms. "Substituted aryl" refers to an aryl moiety substituted with one or more substituent groups, (e.g., tolyl, mesityl and perfluorophenyl) and the terms "heteroatom-containing aryl" and "heteroaryl" refer to aryl in which at least one carbon atom is replaced with a heteroatom.

[0033] The term "aralkyl" refers to an alkyl group with an aryl substituent, and the term "aralkylene" refers to an alkylene group with an aryl substituent; the term "alkaryl" refers to an aryl group that has an alkyl substituent, and the term "alkarylene" refers to an arylene group with an alkyl substituent.

[0034] The terms "halo" and "halogen" are used in the conventional sense to refer to a chloro, bromo, fluoro or iodo substituent. The terms "haloalkyl," "haloalkenyl" or "haloalkynyl" (or "halogenated alkyl," "halogenated alkenyl," or "halogenated alkynyl") refers to an alkyl, alkenyl or alkynyl group, respectively, in which at least one of the hydrogen atoms in the group has been replaced with a halogen atom.

[0035] The term "heteroatom-containing" as in a "heteroatom-containing hydrocarbyl group" refers to a molecule or molecular fragment in which one or more carbon atoms is replaced with an atom other than carbon, e.g., nitrogen, oxygen, sulfur, phosphorus or silicon. Similarly, the term "heteroalkyl" refers to an alkyl substituent that is heteroatom-containing, the term "heterocyclic" refers to a cyclic substituent that is heteroatom-containing, the term "heteroaryl" refers to an aryl substituent that is

heteroatom-containing, and the like. When the term "heteroatom-containing" appears prior to a list of possible heteroatom-containing groups, it is intended that the term apply to every member of that group. That is, the phrase "heteroatom-containing alkyl, alkenyl and alkynyl" is to be interpreted as "heteroatom-containing alkyl, heteroatom-containing alkenyl and heteroatom-containing alkynyl."

5 [0036] "Hydrocarbyl" refers to univalent hydrocarbyl radicals containing 1 to about 30 carbon atoms, preferably 1 to about 24 carbon atoms, most preferably 1 to about 12 carbon atoms, including branched or unbranched, saturated or unsaturated species, such as alkyl groups, alkenyl groups, aryl groups, and the like. The term "lower hydrocarbyl" 10 intends a hydrocarbyl group of one to six carbon atoms, preferably one to four carbon atoms. "Substituted hydrocarbyl" refers to hydrocarbyl substituted with one or more substituent groups, and the terms "heteroatom-containing hydrocarbyl" and "heterohydrocarbyl" refer to hydrocarbyl in which at least one carbon atom is replaced with a heteroatom.

15 [0037] By "substituted" as in "substituted hydrocarbyl," "substituted aryl," "substituted alkyl," "substituted alkenyl" and the like, as alluded to in some of the aforementioned definitions, is meant that in the hydrocarbyl, hydrocarbylene, alkyl, alkenyl or other moiety, at least one hydrogen atom bound to a carbon atom is replaced with one or more substituents that are functional groups such as hydroxyl, alkoxy, thio, phosphino, amino, 20 halo, silyl, and the like. When the term "substituted" appears prior to a list of possible substituted groups, it is intended that the term apply to every member of that group. That is, the phrase "substituted alkyl, alkenyl and alkynyl" is to be interpreted as "substituted alkyl, substituted alkenyl and substituted alkynyl." Similarly, "optionally substituted alkyl, alkenyl and alkynyl" is to be interpreted as "optionally substituted alkyl, optionally 25 substituted alkenyl and optionally substituted alkynyl."

[0038] As used herein the term "silyl" refers to the $-\text{Si}Z^1Z^2Z^3$ radical, where each of Z^1 , Z^2 , and Z^3 is independently selected from the group consisting of hydrido and optionally substituted alkyl, alkenyl, alkynyl, aryl, aralkyl, alkaryl, heterocyclic, alkoxy, aryloxy and amino.

30 [0039] As used herein, the term "phosphino" refers to the group $-\text{P}Z^1Z^2$, where each of Z^1 and Z^2 is independently selected from the group consisting of hydrido and optionally substituted alkyl, alkenyl, alkynyl, aryl, aralkyl, alkaryl, heterocyclic and amino.

[0040] The term "amino" is used herein to refer to the group $-NZ^1Z^2$, where each of Z^1 and Z^2 is independently selected from the group consisting of hydrido and optionally substituted alkyl, alkenyl, alkynyl, aryl, aralkyl, alkaryl and heterocyclic.

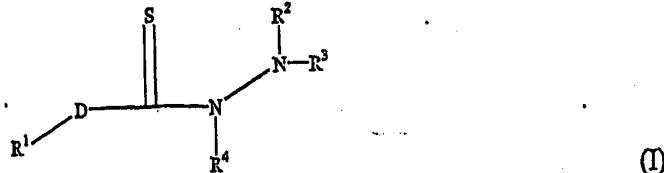
[0041] The term "thio" is used herein to refer to the group $-SZ^1$, where Z^1 is selected from the group consisting of hydrido and optionally substituted alkyl, alkenyl, alkynyl, aryl, aralkyl, alkaryl and heterocyclic.

[0042] As used herein all reference to the elements and groups of the Periodic Table of the Elements is to the version of the table published by the Handbook of Chemistry and Physics, CRC Press, 1995, which sets forth the new IUPAC system for numbering groups.

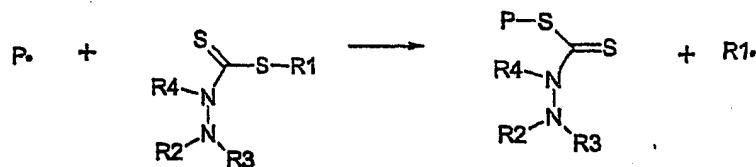
[0043] This invention provides novel compounds and control agents useful for the control of free radical polymerization reactions. In general a free radical polymerization is carried out with these control agents by creating a mixture of at least one polymerizable monomer, the control agent and optionally at least one source of free radicals, e.g., an initiator. The source of free radicals is optional because some monomers may self-initiate upon heating. After or upon forming the polymerization mixture, the mixture is subjected to polymerization conditions. Polymerization conditions are those conditions that cause the at least one monomer to form at least one polymer, as discussed herein, such as temperature, pressure, atmosphere, ratios of starting components used in the polymerization mixture, reaction time or external stimuli of the polymerization mixture.

Control Agents

[0044] Generally, the control agents of this invention may be characterized by the general formula (I') above. More specifically, the control agents of this invention may be characterized by the general formula:



wherein D is S, Te or Se. Preferably, D is sulfur. R^1 is generally any group that can be easily expelled under its free radical form ($R^{1\bullet}$) upon an addition-fragmentation reaction, as depicted below in Scheme 1 (showing D as S):



Scheme 1

[0045] In Scheme 1, P is a free radical, typically a macro-radical, such as polymer chain. More specifically, R¹ is selected from the group consisting of hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof. Even more specifically, R¹ is selected from the group consisting of optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted alkoxyl, optionally substituted heterocyclyl, optionally substituted alkylthio, optionally substituted amino and optionally substituted polymer chains. And still more specifically, R¹ is selected from the group consisting of –CH₂Ph,

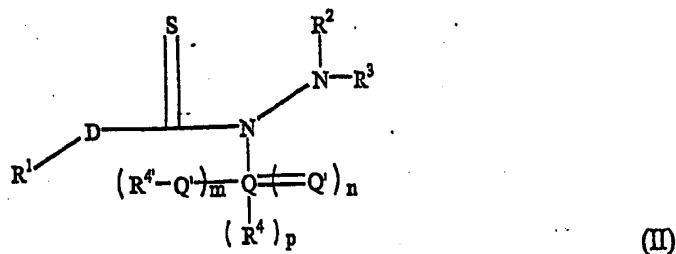
–CH(CH₃)CO₂CH₂CH₃, –CH(CO₂CH₂CH₃)₂, –C(CH₃)₂CN, –CH(Ph)CN and –C(CH₃)₂Ph.

[0046] Also, R² and R³ are each independently selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof. More specifically, R² and R³ may be each independently selected from the group consisting of hydrogen, optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted acyl, optionally substituted, aroyl, optionally substituted alkoxy, optionally substituted heteroaryl, optionally substituted heterocyclyl, optionally substituted alkylsulfonyl, optionally substituted alkylsulfinyl, optionally substituted alkylphosphonyl, optionally substituted arylsulfinyl, and optionally substituted arylphosphonyl. Specific embodiments of R² and/or R³ are listed in the above definitions, and in addition include perfluorinated aromatic rings, such as perfluorophenyl. Also optionally, R² and R³ can together form a double bond alkenyl moiety off the nitrogen atom, and in that case R² and R³ are together optionally substituted alkenyl moieties.

[0047] Finally, R⁴ is selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof; and optionally, R⁴ combines with R²

and/or R^3 to form a ring structure, with said ring having from 3 to 50 non-hydrogen atoms. In particular, R^4 is selected from the group consisting of hydrogen, optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted acyl, optionally substituted aroyl, amino, thio, optionally substituted aryloxy and optionally substituted alkoxy. Preferred R^4 groups include methyl and phenyl.

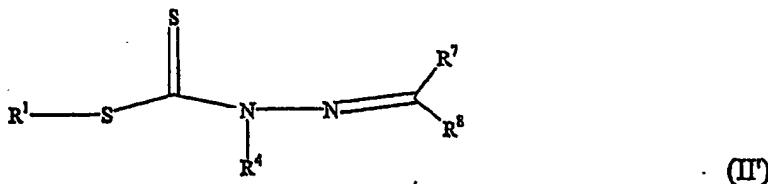
[0048] In a more specific embodiment, a bulky moiety is attached to the N^1 nitrogen atom, which in some embodiments may be characterized by the general formula:



10 wherein D and R^1 - R^4 are as defined above and Q is selected from the group consisting of carbon, sulfur and phosphorus (C, S and P); Q' is selected from the group consisting of oxygen and sulfur (O and S); R^4 is typically selected from the same group as R^4 ; and n, m and p are each either 0, 1 or 2 to satisfy the valency of Q. Thus, for example, when Q is carbon, n and p may both be 1 and m is 0. Another example for when Q is carbon is that n is 1 and m is 1 and p is 0. Also for example, when Q is phosphorus, n is 1 and m is 2. Also for example, when Q is sulfur, n is 1 or 2, but typically 2; and m is typically 0 and p is 1. In some preferred embodiments, Q is carbon or sulfur and Q' is oxygen. In these preferred embodiments, R^4 and R^4 are each independently more preferably selected from the group consisting of optionally substituted alkyl and optionally substituted aryl.

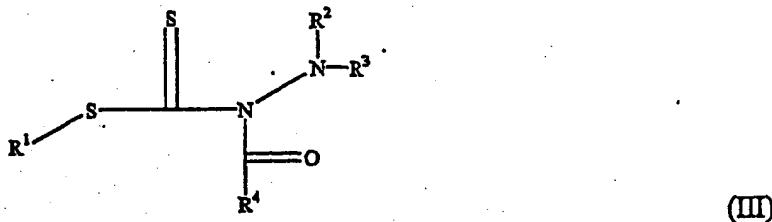
20 [0049] In some embodiments within formulas (I) and (II), above, R^2 and/or R^3 may be independently selected from $-Q(Q')_n(R^4-Q')_m(R^4)_p$, which is the moiety from the N^1 atom in formula (II), with the N^1 atoms being identified in formula (I'). In these embodiments, Q, Q', R^4 , R^4 , n, m and p have the above stated definitions.

25 [0050] In embodiments that involve emulsions, the R^2 and R^3 preferably together form a double bond alkenyl moiety off the nitrogen atom, and in that case R^2 and R^3 are together optionally substituted alkenyl. In these embodiments, the control agents of this invention may be characterized by the general formula:



wherein R¹ and R⁴ are defined above and R⁷ and R⁸ are each independently selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof. More specifically, R⁷ and R⁸ may be each independently selected from the group consisting of hydrogen, optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted acyl, optionally substituted, aroyl, optionally substituted alkoxy, optionally substituted heteroaryl, optionally substituted heterocycl, optionally substituted alkylsulfonyl, optionally substituted alkylsulfinyl, optionally substituted alkylphosphonyl, optionally substituted arylsulfinyl, and optionally substituted arylphosphonyl. Specific embodiments of R⁷ and/or R⁸ are listed in the above definitions, and in addition include perfluorenated aromatic rings, such as perfluorophenyl. Preferred embodiments of R⁷ and/or R⁸ include methyl and phenyl.

[0051] Some of the control agents are novel compounds. In some embodiments, the novel compounds may be characterized by the above formula (II). More specifically, novel compounds may be characterized by the formula:



wherein R¹ is selected from the group consisting of hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof, with the proviso that R¹ is not methyl;

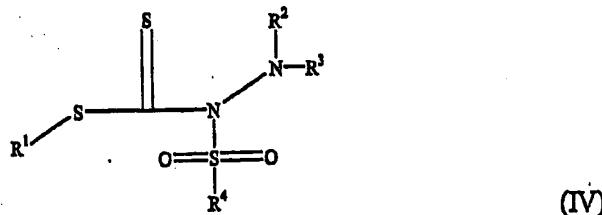
[0052] R² and R³ are each independently selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof; and

[0053] R⁴ is selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing

hydrocarbyl, and combinations thereof, and optionally, R⁴ combines with R² to form a ring structure, with said ring having from 3 to 50 non-hydrogen atoms. In more specific embodiments, R¹-R⁴ are selected from the lists given above.

[0054] In some embodiments within formula (III), R² and/or R³ may be independently selected from $-Q(=Q')_n(R^{4'}-Q')_m(R^4)_p$. In these embodiments, Q, Q', R⁴, R^{4'}, n, m and p have the above stated definitions.

[0055] Also more specifically, the novel compounds may be characterized by the formula:



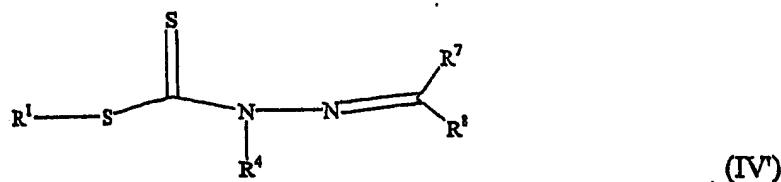
10 wherein R¹ is selected from the group consisting of hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof;

[0056] R² and R³ are each independently selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof, and optionally, R² and R³ are joined together in a ring structure having between 3 and 50 non-hydrogen atoms in said ring; and

[0057] R⁴ is selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof; and optionally, R⁴ combines with R² to form a ring structure, with said ring having from 3 to 50 non-hydrogen atoms. In more specific embodiments, R¹-R⁴ are selected from the lists given above.

[0058] In some embodiments within formula (IV), R² and/or R³ may be independently selected from $-Q(=Q')_n(R^{4'}-Q')_m(R^4)_p$. In these embodiments, Q, Q', R⁴, R^{4'}, n, m and p have the above stated definitions.

[0059] In other embodiments, the novel compounds include those characterized by the general formula:



wherein R¹ is selected from the group consisting of hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof, with the proviso that R¹ is not methyl;

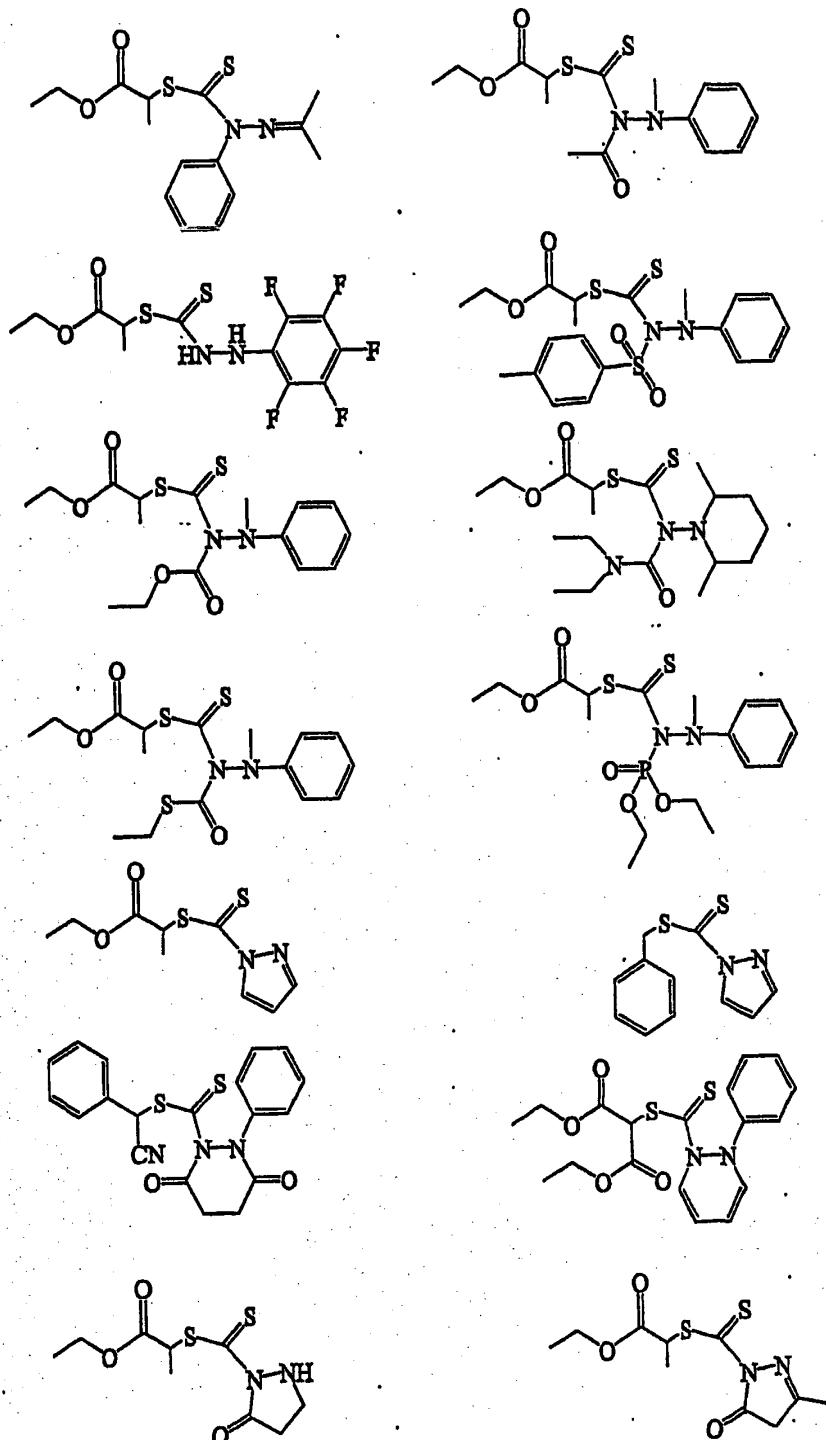
5 [0060] R⁷ and R⁸ are each independently selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof; and

[0061] R⁴ is selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof. In more specific embodiments, R¹, R⁷, R⁸ and R⁴ are selected from the lists given above.

[0062] In more specific embodiments, the groups of the novel compounds can have R¹ is selected from the group consisting of optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted alkoxy, optionally substituted heterocycl, optionally substituted alkylthio, optionally substituted amino and optionally substituted polymer chains. Even more specifically, R¹ is selected from the group consisting of -CH₂Ph, -CH(CH₃)CO₂CH₂CH₃,

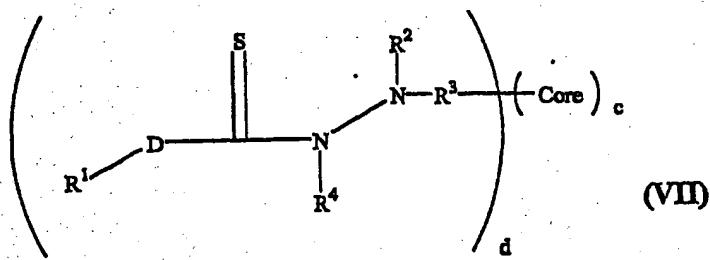
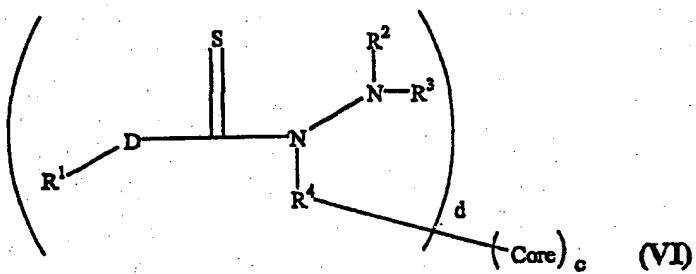
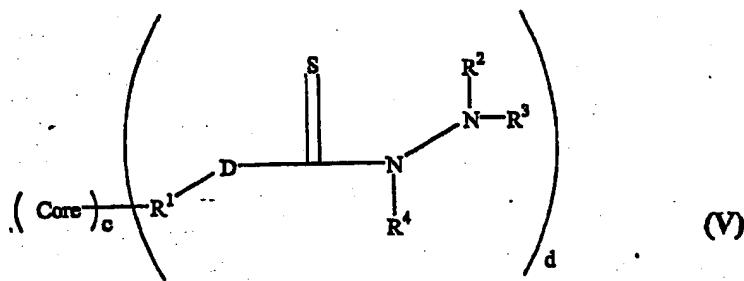
-CH(CO₂CH₂CH₃)₂, -C(CH₃)₂CN, -CH(Ph)CN and -C(CH₃)₂Ph. Also, R² and R³ may be each independently selected from the group consisting of hydrogen, optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted acyl, optionally substituted aroyl, optionally substituted alkoxy, optionally substituted heteroaryl, optionally substituted heterocycl, optionally substituted alkylsulfonyl, optionally substituted alkylsulfinyl, optionally substituted alkylphosphonyl, optionally substituted arylsulfinyl, and optionally substituted arylphosphonyl. Further, R⁴ may be selected from the groups listed above.

[0063] Specific control agents within these formulas include:



[0064] This invention also includes multi-functional control agents and their use in free radical polymerization. A multi-functional control agent is a molecule that allows for two or more polymer chains to polymerize from a single control agent molecule. In

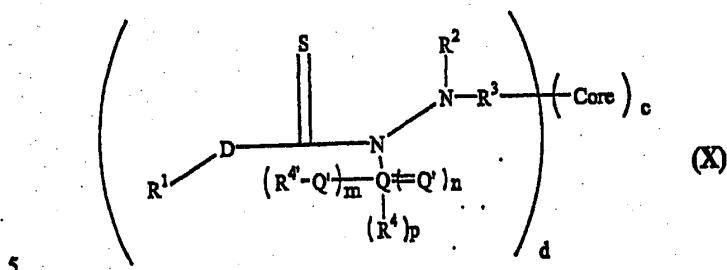
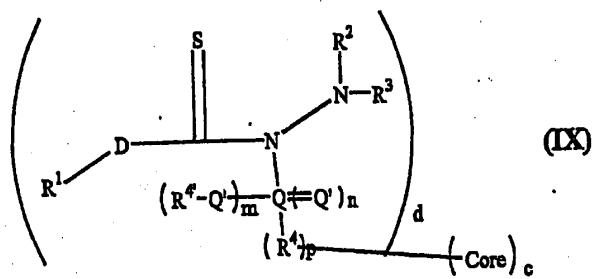
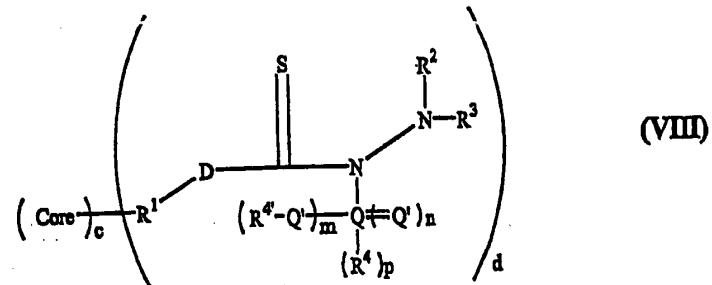
some embodiments, the control agents are attached to a core that has multiple functional sites for attachment of one portion of a control agent. Thus, in some embodiments, R^2 , R^3 and/or R^4 forms part of or is attached to a core molecule. In other embodiments, R^1 is part of or attached to a core molecule. These multi-functional chain transfer agents may 5 be characterized by any of the following general formulas:



wherein Core is a core molecule, and D, R^1 , R^2 , R^3 and R^4 are as defined above, c is 1 or 10 more and d is 2 or more. Formulas (V), (VI) and (VII) include multiple core molecules, providing many possible points from which a free radical polymerization may be controlled. This provides the ability to make many different architectures for polymers, some of which are discussed below. For example, for a star architecture polymer c is 1 and d is 3 for a three arm star; c is 1 and d is 4 for a 4 arm star; c is 1 and d is 6 for a six

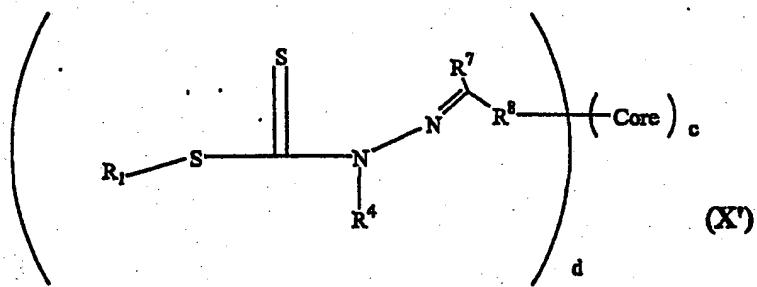
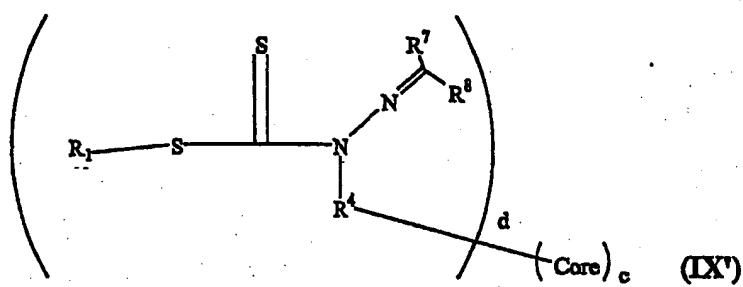
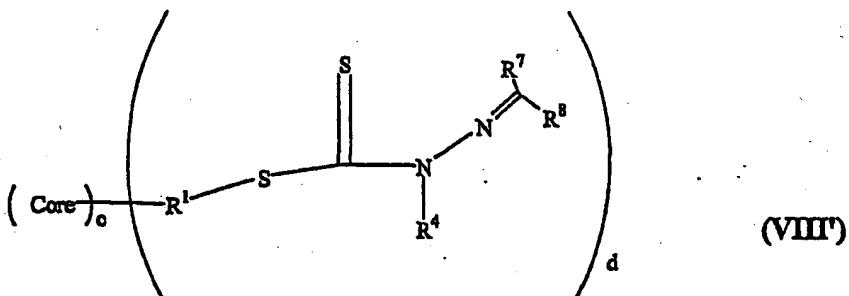
arm star; etc. Also for example, for a grafted polymer, c is 1 and d is 2 for two grafts, etc. For a hyper-branched polymer, c is 2 or more and d is 2 or more.

[0065] The multifunctional chain transfer agents may also be drawn for the more specific embodiments of this invention, as follows:



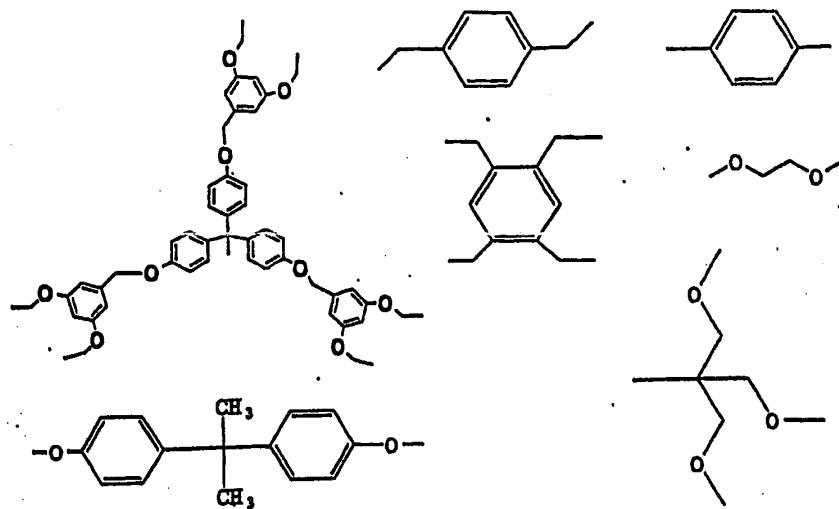
wherein Core, Q, Q', n, c, d, D, R¹, R², R³ and R⁴ are as defined above.

[0066] The multi-functional control agents may be characterized by any of the following general formulas for the emulsion embodiment:



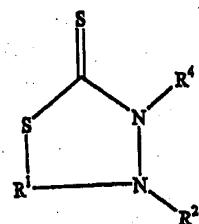
wherein Core is a core molecule, and R^1 , R^4 , R^7 and R^8 are as defined above, c is 1 or more and d is 2 or more.

5 [0067] The Core molecule may be selected from the group consisting of dendritic molecules, small molecules and polymers with at least two terminus ends. Thus, Core molecule may be optionally substituted hydrocarbyl and optionally substituted heteroatom containing hydrocarbyl. Specific examples of Core molecules include:

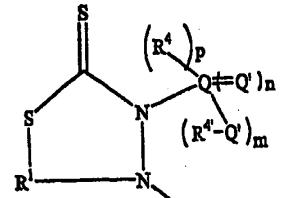


[0068] In other embodiments, the Core will be a polymer chain. These embodiments allow for the preparation of grafts or block copolymers by attaching control agents to two or more points along the polymer backbone or side chains or polymer termini.

[0069] In alternative embodiments, the control agents of this invention have a ring structure, which upon ring opening may form a multi-functional control agent. Thus, in some embodiments, formulas (I) and (II) above are arranged so that D is sulfur, R³ is deleted, and the nitrogen atom from which R³ was deleted forms a ring with R¹ providing general formulas:

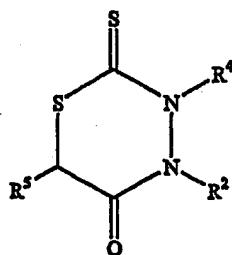


(XI) and

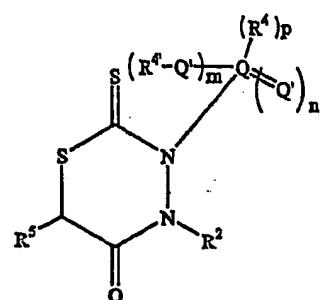


(XII)

wherein the above variables have the same definitions, with the exception that R¹ is a bifunctional moiety within the definitions given above. In a particularly preferred embodiment, R¹ comprises -CH(R⁵)-C(O)— such that formulas (XI) and (XII) can be redrawn as:



(XIII) and

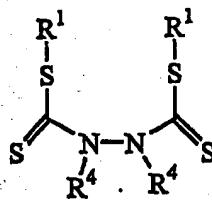


(XIV)

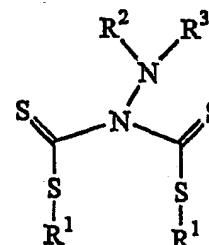
wherein R^2 , R^4 , Q , Q' and n are as defined above. R^5 is selected from the group consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof. In particular, R^5 is selected from the group consisting of hydrogen, optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted acyl, optionally substituted, aroyl, and optionally substituted alkoxy. Preferred R^5 groups include hydrogen, methyl, ethyl, propyl, butyl, methoxy, ethoxy, propoxy, phenoxy and phenyl. As above, R^4 and R^2 can combine to form a ring structure having from 4 to 50 non-hydrogen atoms.

[0070] In some embodiments within formulas (XIII) and (XIV), R^2 may be independently selected from $-Q(=Q')_n(R^4-Q')_m(R^4)_p$. In these embodiments, Q , Q' , R^4 , R^4 , n , m and p have the above stated definitions.

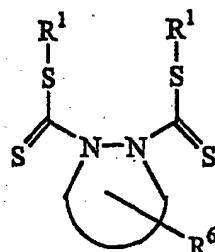
[0071] In other alternative embodiments, the multi-functional control agents of this invention can be characterized by any of the following formulas (which may fall within the general formulas given above):



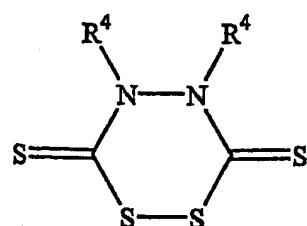
(XV)



(XVII)



(XVI)



(XVIII)

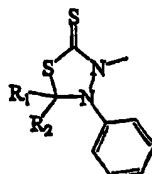
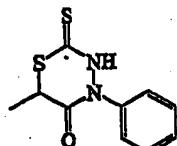
wherein R¹, R², R³ and R⁴ are as defined above. In formula (XVI), the moiety



R⁶ refers to a ring structure having between 3 and 20 non-hydrogen atoms in the ring, including single ring or multiple rings that are fused together, linked covalently, or linked to a common group such as a methylene or ethylene moiety. R⁶ is a substituent on any member of the ring other than the two shown nitrogen atoms. There may be as many R⁶ substituents as ring members in addition to the two nitrogen atoms. R⁶ substituents may be selected from the group consisting of hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations thereof. In particular, R⁶ is selected from the group consisting of optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted acyl, optionally substituted, aroyl, and optionally substituted alkoxy.

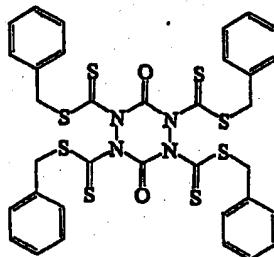
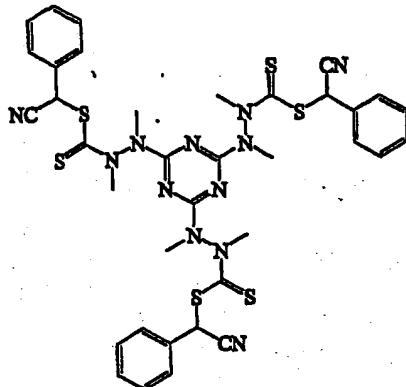
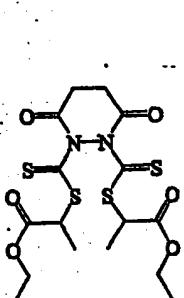
[0072] Specific cyclic/multi-functional control agents include:

Cyclic

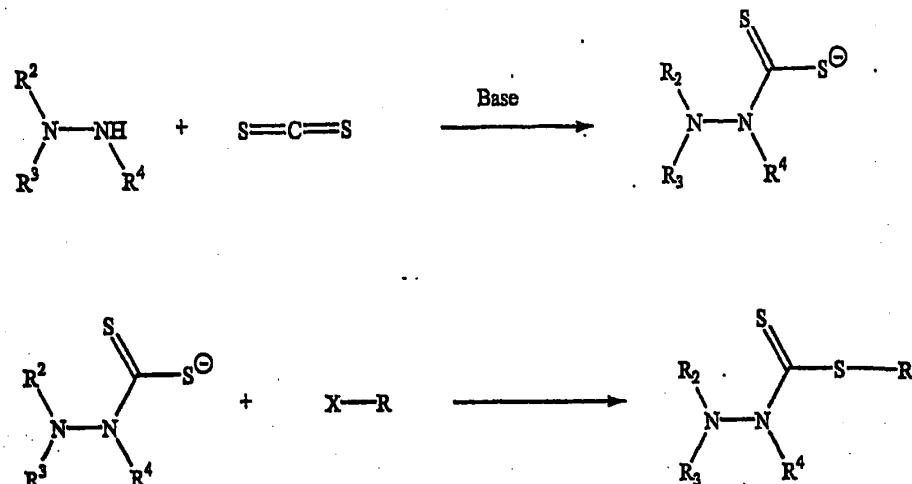


$R_1 = H$
 $R_2 = CN, CO_2Et, Ph$

Multi-functional



[0073] The control agents of this invention are synthesized, generally, by methods known to those of skill in the art. The general synthetic approach comprises the nitrogen nucleophilic addition to carbon disulfide and alkylation of the resulted dihiocarbamate with alkylhalides in a one-pot methodology, as shown in the following scheme 2:



[0074] This method is similar to those published in scientific journals, e.g., Castro et al., *J. Org. Chem.*, 1984, 49, 863, which is incorporated herein by reference.

[0075] The synthesis conditions optimized for these particular nucleophiles — hydrazines and their derivatives include: temperature in the range of 0 °C to ambient; solvents — alcohols, acetone, acetonitrile, dioxane, DMF, DMSO; base — sodium hydroxide, potassium hydroxide, and sodium hydride. The preferred conditions include using sodium hydroxide as the base in DMSO at ambient temperature.

[0076] The general procedure comprises starting with the hydrazine or its derivative dissolved in DMSO in approximately a 0.5-1.0 M concentration at ambient temperature. The solution is then treated with approximately 1 equivalent of NaOH and followed by addition of approximately 1 equivalent of carbon disulfide. The resulting solution is then stirred (for example, for approximately 1 hour at ambient temperature) before addition of approximately 1 equivalent of an alkylation agent. Work-up may comprise addition of water, extraction with organic solvent, and drying. The desired control agent may be purified by chromatography and/or recrystallization and may be characterized by ¹H NMR, ¹³C NMR, and GC/MS.

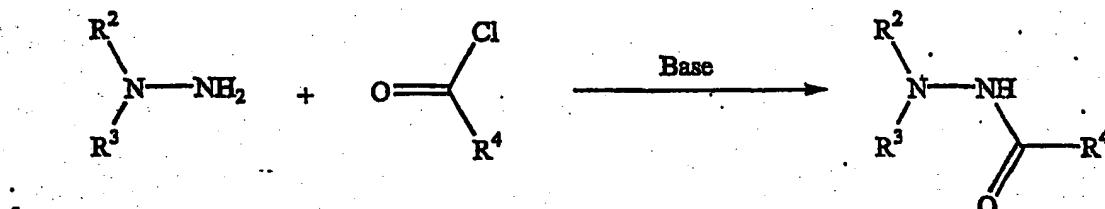
[0077] Most of hydrazines and their derivatives are available commercially from known chemical sources. However, to increasing the diversity of the control agents, several transformations may be applied, including:

a) hydrazone formation as shown in scheme 3:



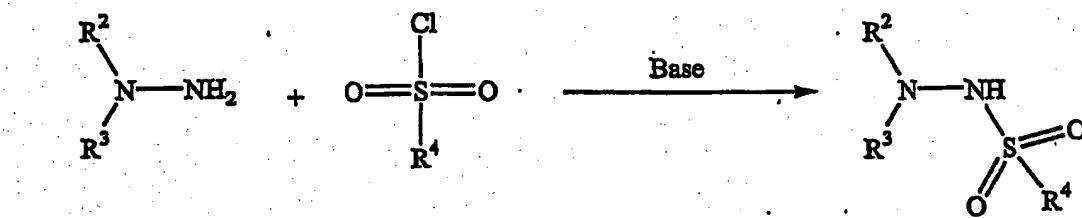
Scheme 3

b) hydrazide formation as shown in scheme 4:



Scheme 4

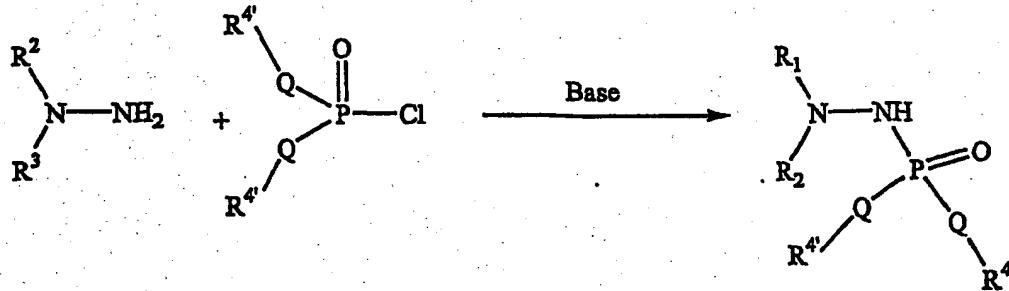
c) sulfonylhydrazine formation as shown in scheme 5:



10

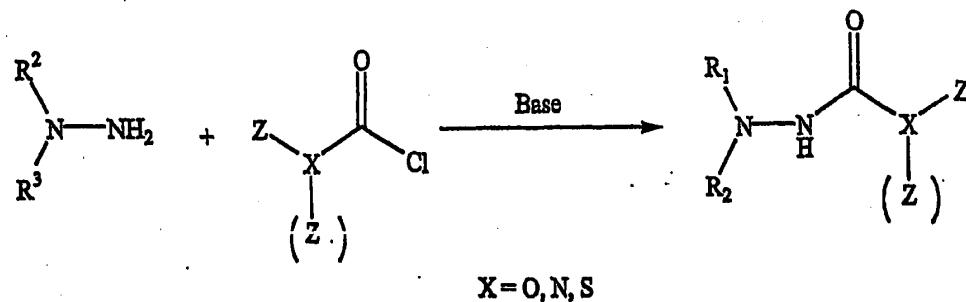
Scheme 5

d) phosphoryl hydrazine formation as shown in scheme 6:



Scheme 6

15 e) Urea and urethane derivatives formation as shown in scheme 7:

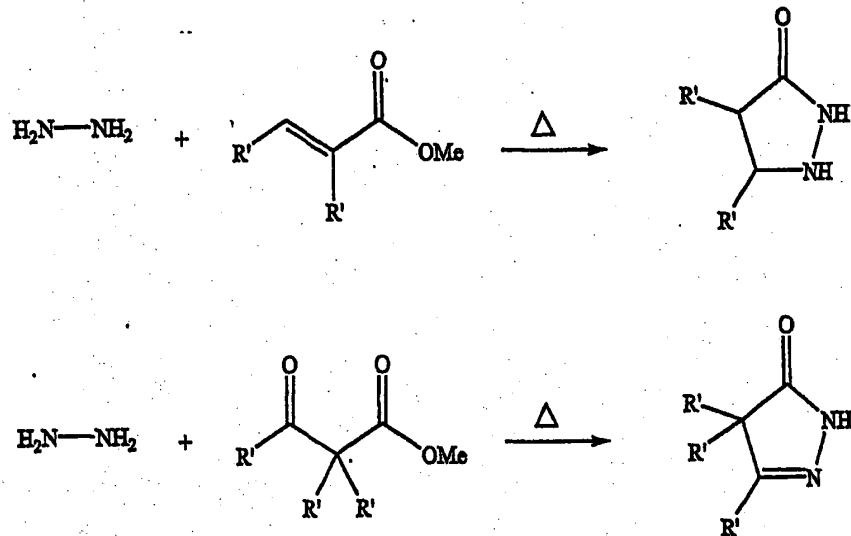


$\text{X} = \text{O}, \text{N}, \text{S}$

Scheme 7

[0078] In scheme 7, Z is used to denote the variables shown in formula (II), above.

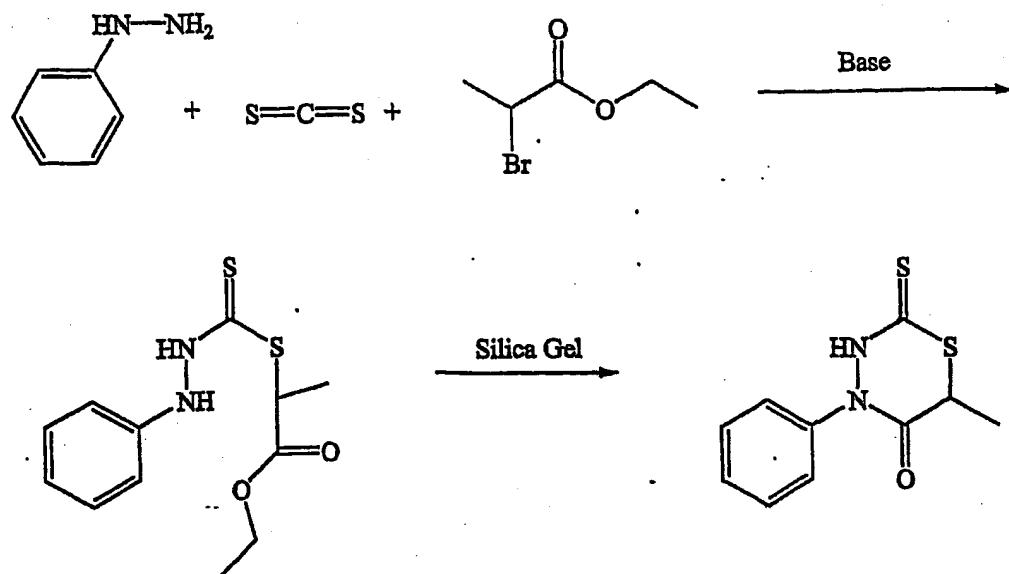
[0079] Cyclic hydrazine derivatives formation as shown in scheme 8:



Scheme 8

[0080] In scheme 8, R' is used to represent the various R groups discussed herein (e.g., R^2 , R^3 and/or R^4).

[0081] The cyclic control agents for example as shown below may be prepared from an appropriate alkylation agent which can subsequently react with another nitrogen of the hydrazine, as shown below in scheme 9:



Scheme 9

[0082] Those of skill in the art will appreciate that scheme 9 can be modified to obtain desired substituents, as shown in generally in formulas (XIII) and (XIV), above.

5

Polymerization Processes

[0083] The polymerization conditions that may be used include temperatures for polymerization typically in the range of from about 20°C to about 110°C, more preferably in the range of from about 50°C to about 90°C and even more preferably in the range of from about 60°C to about 80°C. The atmosphere may be controlled, with an inert atmosphere being preferred, such as nitrogen or argon. The molecular weight of the polymer is controlled via adjusting the ratio of monomer to control agent. Generally, the molar ratio of monomer to control agent is in the range of from about 5 to about 5000, more preferably in the range of from about 10 to about 2000, and most preferably from 10 to about 1500.

[0084] A free radical source is provided in the polymerization mixture, which can stem from spontaneous free radical generation upon heating or preferably from a free radical initiator. In the latter case the initiator is added to the polymerization mixture at a concentration high enough to for an acceptable polymerization rate (e.g., commercially significant conversion in a certain period of time, such as listed below). Conversely, a too high free radical initiator to control agent ratio will favor unwanted dead polymer formation through radical-radical coupling reaction leading to polymer materials with

uncontrolled characteristics. The molar ratio of free radical initiator to control agent for polymerization are typically in the range of from about 2:1 to about 0.02:1.

[0085] Polymerization conditions also include the time for reaction, which may be from about 0.5 hours to about 72 hours, preferably in the range of from about 1 hour to about

5 24 hours, more preferably in the range of from about 2 hours to about 12 hours.

Conversion of monomer to polymer is preferably at least about 50%, more preferably at least about 75% and most preferable at least about 85%.

[0086] The polymerization process generally proceeds in a "living" type manner. Thus, generally an approximately linear relationship between conversion and number average molecular weight can be observed, although this is not a pre-requisite. The living character manifests itself by the ability to prepare block copolymers: hence, a polymer chain is first grown with monomer A, and then, when monomer A is depleted, monomer B is added to extend the first block of polymer A with a second block of polymer B.

10 Thus, in some instances, particularly when the chain transfer constant of the control agent, C_t , is low (C_t being defined as the ratio of the transfer rate coefficient to the propagation rate constant), e.g., C_t less than 2, the molecular weight to conversion plot might not exhibit a linear trend: this does not preclude however that block copolymer formation did not occur. Block copolymer formation through a living process can be demonstrated using analytical techniques such as polymer fractionation with selective solvent (of polymer A, polymer B, respectively), gradient elution chromatography and/or 2-dimensional chromatography. Block copolymers tend to microphase-separate and organize in a variety of morphologies that can be probed by physical techniques such as X-ray diffraction, dynamic mechanical testing, and the like.

[0087] Initiators, as discussed above, may be optional. When present, initiators useful in the polymerization mixture and the inventive process are known in the art, and may be selected from the group consisting of alkyl peroxides, substituted alkyl peroxides, aryl peroxides, substituted aryl peroxides, acyl peroxides, alkyl hydroperoxides, substituted alkyl hydroperoxides, aryl hydroperoxides, substituted aryl hydroperoxides, heteroalkyl peroxides, substituted heteroalkyl peroxides, heteroalkyl hydroperoxides, substituted heteroalkyl hydroperoxides, substituted heteroalkyl hydroperoxides, heteroaryl peroxides, substituted heteroaryl peroxides, heteroaryl hydroperoxides, substituted heteroaryl hydroperoxides, alkyl peresters, substituted alkyl peresters, aryl peresters, substituted aryl peresters, and azo compounds. Specific initiators include benzoylperoxide (BPO) and AIBN. The polymerization

mixture may use a reaction media is typically either an organic solvent or bulk monomer or neat. Optionally, after the polymerization is over (e.g., completed or terminated) the thio-moiety (e.g., a dithio-moiety) of the control agent can be cleaved by chemical or thermal ways, if one wants to reduce the sulfur content of the polymer and prevent any problems associated with presence of the control agents chain ends, such as odor or discoloration. Typical chemical treatment includes the catalytic or stoichiometric addition of base such as a primary amine, acid or anhydride, or oxidizing agents such as hypochlorite salts.

[0088] Generally, monomers that may be polymerized using the methods of this invention (and from which M, below, may be derived) include at least one monomer selected from the group consisting of styrene, substituted styrene, alkyl acrylate, substituted alkyl acrylate, alkyl methacrylate, substituted alkyl methacrylate, acrylonitrile, methacrylonitrile, acrylamide, methacrylamide, N-alkylacrylamide, N-alkylmethacrylamide, N,N-dialkylacrylamide, N,N-dialkylmethacrylamide, isoprene, butadiene, ethylene, vinyl acetate and combinations thereof. Functionalized versions of these monomers may also be used. Specific monomers or comonomers that may be used in this invention include methyl methacrylate, ethyl methacrylate, propyl methacrylate (all isomers), butyl methacrylate (all isomers), 2-ethylhexyl methacrylate, isobornyl methacrylate, methacrylic acid, benzyl methacrylate, phenyl methacrylate, methacrylonitrile, α -methylstyrene, methyl acrylate, ethyl acrylate, propyl acrylate (all isomers), butyl acrylate (all isomers), 2-ethylhexyl acrylate, isobornyl acrylate, acrylic acid, benzyl acrylate, phenyl acrylate, acrylonitrile, styrene, glycidyl methacrylate, 2-hydroxyethyl methacrylate, hydroxypropyl methacrylate (all isomers), hydroxybutyl methacrylate (all isomers), N,N-dimethylaminoethyl methacrylate, N,N-diethylaminoethyl methacrylate, triethyleneglycol methacrylate, itaconic anhydride, itaconic acid, glycidyl acrylate, 2-hydroxyethyl acrylate, hydroxypropyl acrylate (all isomers), hydroxybutyl acrylate (all isomers), N,N-dimethylaminoethyl acrylate, N,N-diethylaminoethyl acrylate, triethyleneglycol acrylate, methacrylamide, N-methylacrylamide, N,N-dimethylacrylamide, N-tert-butylmethacrylamide, N-n-butylmethacrylamide, N-methylolemethacrylamide, N-ethylolmethacrylamide, N-tert-butylacrylamide, N-n-butylacrylamide, N-methylolemacrylamide, N-ethylolacrylamide, 4-acryloylmorpholine, vinyl benzoic acid (all isomers), diethylaminostyrene (all isomers), α -methylvinyl benzoic acid (all isomers), diethylamino α -methylstyrene (all isomers), p-

vinylbenzene sulfonic acid, p-vinylbenzene sulfonic sodium salt, trimethoxysilylpropyl methacrylate, triethoxysilylpropyl methacrylate, tributoxysilylpropyl methacrylate, dimethoxymethylsilylpropyl methacrylate, diethoxymethylsilylpropyl methacrylate, dibutoxymethylsilylpropyl methacrylate, diisopropoxymethylsilylpropyl methacrylate, 5 dimethoxysilylpropyl methacrylate, diethoxysilylpropyl methacrylate, dibutoxysilylpropyl methacrylate, diisopropoxysilylpropyl methacrylate, trimethoxysilylpropyl acrylate, triethoxysilylpropyl acrylate, tributoxysilylpropyl acrylate, dimethoxymethylsilylpropyl acrylate, diethoxymethylsilylpropyl acrylate, dibutoxymethylsilylpropyl acrylate, diisopropoxymethylsilylpropyl acrylate, 10 dimethoxysilylpropyl acrylate, diethoxysilylpropyl acrylate, dibutoxysilylpropyl acrylate, diisopropoxysilylpropyl acrylate, maleic anhydride, N-phenylmaleimide, N-butylmaleimide, butadiene, isoprene, chloroprene, ethylene, vinyl acetate and combinations thereof.

[0089] In some embodiments of the polymers of this invention, a combination of 15 hydrophobic and hydrophilic monomers may be used, either randomly or in separate blocks of a copolymer (e.g., thermoplastic elastomers, grafts, etc). The hydrophobic/hydrophilic nature of monomers may be determined according to the log P of the particular monomers, which is sometimes referred to as the octanol-water partition coefficient. Log P values are well known and are determined according to a standard test 20 that determines the concentration of monomer in a water/1-octanol separated mixture. In particular, computer programs are commercially available as well as on the internet that will estimate the log P values for particular monomers. Some of the log P values in this application were estimated from the web site

<http://esc.syrres.com/interkow/kowdemo.htm>, which provides an estimated log P value 25 for molecules by simply inserting the CAS registry number or a chemical notation. Log P values listed herein were obtained from either the web site listed above or from Hansch et al. *Exploring QSAR: Hydrophobic, Electronic, and Steric Constants* (ACS Professional Reference Book, 1995), which is incorporated herein by reference.

[0090] Suitable hydrophilic monomers (with approximate log P values listed in 30 parentheses) may be listed above and include, but are not limited to, acrylic acid (0.35), methacrylic acid (0.93), N,N-dimethylacrylamide (-0.13), dimethyl aminoethyl methacrylate (0.97), quaternized dimethylaminoethyl methacrylate, methacrylamide (-0.26), N-t-butyl acrylamide (1.02), maleic acid (-0.48), maleic anhydride and its half

esters, crotonic acid (0.72), itaconic acid (-0.34), acrylamide (-0.67), acrylate alcohols, hydroxyethyl methacrylate, diallyldimethyl ammonium chloride, vinyl ethers (such as methyl vinyl ether), maleimides, vinyl pyridine, vinyl imidazole (0.96), other polar vinyl heterocyclics, styrene sulfonate, allyl alcohol (0.17), vinyl alcohol (such as that produced by the hydrolysis of vinyl acetate after polymerization), salts of any acids and amines listed above, and mixtures thereof. Preferred hydrophilic monomers include acrylic acid, N,N-dimethyl acrylamide (-0.13), dimethylaminoethyl methacrylate (0.97), quaternized dimethyl aminoethyl methacrylate, vinyl pyrrolidone, salts of acids and amines listed above, and combinations thereof.

5 [0091] Suitable hydrophobic monomers may be listed above and include, but are not limited to, acrylic or methacrylic acid esters of C₁ -C₁₈ alcohols, such as methanol, ethanol, methoxy ethanol, 1-propanol, 2-propanol, 1-butanol, 2-methyl-1-propanol, 1-pentanol, 2-pentanol, 3-pentanol, 2-methyl-1-butanol, 1-methyl-1-butanol, 3-methyl-1-butanol, 1-methyl-1-pentanol, 2-methyl-1-pentanol, 3-methyl-1-pentanol, t-butanol (2-methyl-2-propanol), cyclohexanol, neodecanol, 2-ethyl-1-butanol, 3-heptanol, benzyl alcohol, 2-octanol, 6-methyl-1-heptanol, 2-ethyl-1-hexanol, 3,5-dimethyl-1-hexanol, 3,5,5-tri methyl-1-hexanol, 1-decanol, 1-dodecanol, 1-hexadecanol, 1-octa decanol, and the like, the alcohols having from about 1 to about 18 carbon atoms, preferably from about 1 to about 12 carbon atoms; styrene; polystyrene macromer, vinyl acetate; vinyl chloride; vinylidene chloride; vinyl propionate; alpha-methylstyrene; t-butylstyrene; butadiene; cyclohexadiene; ethylene; propylene; vinyl toluene; and mixtures thereof. Preferred hydrophobic monomers (with approximate log P values listed in parentheses) include n-butyl methacrylate (2.36), isobutyl methacrylate (2.66), t-butyl acrylate (2.09), t-butyl methacrylate (2.54), 2-ethylhexyl methacrylate (4.09), methyl methacrylate (1.38), vinyl acetate (0.73), vinyl acetamide, vinyl formamide, and mixtures thereof, more preferably t-butyl acrylate, t-butyl methacrylate, or combinations thereof.

10 [0092] In addition, monomers that polymerize in a ring closing method may also be used in this invention, including monomers that are of the formula:

15 $\text{CH}_2=\text{CH-X'-CH=CH}_2$ where X' comprises from 1 to 20 non-hydrogen atoms. Such monomers are well known in the art. A specific example is

20 $\{\text{CH}_2=\text{CH-N}(\text{CH}_3)_2\text{-CH=CH}_2\}^+ \{\text{Cl}^-\}$.

Emulsion Polymerization Processes

[0093] In the broadest sense, an emulsion polymerization is any heterogeneous polymerization in an aqueous environment. Typically, these systems produce particles of polymer as product. Those skilled in the art recognize many variants of these 5 heterogeneous polymerizations, including true emulsions, micro emulsions, mini emulsions, suspensions and dispersions. These processes are generally distinguished by differences in process, components or results, with specific factors including the presence, amount and type of surfactant required; presence, amount and type of initiator; presence, type and amount of monomer, including monomer solubility; polymerization 10 kinetics; temperature; order of addition of the components, including the timing of addition of the components (e.g., monomer); solubility of the polymeric product; agitation; presence of co-solvents; resulting particle size; particle stability in the polymerization system toward coagulation or sedimentation; and other factors known to those skilled in the art. In some embodiments of this invention, systems that employ a 15 shearing force or step to create small particle sizes are excluded.

[0094] One specifically preferred embodiment of the invention is a controlled heterogeneous polymerization reaction in an emulsion characterized by particle sizes ranging from 20 to 1000 nm, and preferably from 30 to 600 nm or from 40 to 300 nm. Polymerizations of this embodiment may have process parameters similar to those 20 discussed above for "traditional" or "true" emulsion polymerizations. These emulsions are stable (on the order of many months with no observed coagulation or sedimentation), yet are prepared using surfactant in amounts less than 3 % by weight to monomer.

[0095] The use of control agents under emulsion conditions offers other benefits 25 associated with living kinetics (e.g., linear increase in molecular weight as a function of conversion). The controlled free radical emulsion polymerizations of the invention provide a high degree of control over molecular weight, especially at high molecular weight, (as high as $\geq 20,000$, or even $\geq 100,000$), often with narrow molecular weight distribution (polydispersity (M_w/M_n) generally less than 2 and preferably between 1.1 and 1.8).

[0096] In the heterogeneous polymerization process of this invention, the control agent 30 is combined with water, optionally surfactant, initiator, and at least one monomer. Polymerization conditions include a temperature in the range of from about 25°C to

about 150°C, preferably between about 35°C and about 110°C, more preferably between about 50°C and about 100°C, and most preferably between about 60°C and about 90°C. [0097] Polymerization conditions also include a pressure between about ambient pressure up to about 100 atmospheres. Polymerization conditions also include the time for reaction, which may be from about 0.5 hours to about 72 hours, preferably in the range of from about 1 hour to about 24 hours, more preferably in the range of from about 2 hours to about 12 hours.

[0098] Surfactants can be useful in the processes and composition of this invention. Suitable surfactants include any species or mixture of species capable of stabilizing colloidal emulsions. Generally surfactants are amphiphilic molecules comprising both hydrophobic and hydrophilic regions, which are capable of adsorbing to surfaces. Surfactants may be small molecules or polymers, micelle forming or non-micelle forming and may be anionic, cationic, zwitterionic or nonionic. In some embodiments, it may be desirable to use mixtures of surfactants, for example to enhance particle stability or control particle formation. Surfactants can play an important role in determining particle size, particle distribution, particle formation and the stability of the resulting polymer emulsion, which are factors that those of skill in the art typically consider when choosing a surfactant for any specific embodiment. Typical amounts of surfactants range from about 0.01 to about 200 % by weight relative to the monomer, with a more preferred range being from about 0.1 to about 5 % by weight and more specifically preferred being from about 0.5 to about 3 % by weight.

[0099] Suitable surfactants include anionic, small molecule surfactants including substituted or unsubstituted hydrocarbyl sulfates, sulfonates, carboxylates, phosphonates and phosphates, having between 6 and 30 carbon atoms per anionic functional group. When the hydrocarbyl group is substituted, it may have one or more hydrogen or carbon atoms replaced with another atom selected from the group consisting of N, S, O, Si, F, Cl, Br and I. The hydrocarbyl may also have one or more hydrogen or carbon atom replaced with a functionality such as a keto, ester, amide, ether, thioether and the like. Specific examples of anionic, non-polymeric surfactants include sodium dodecyl sulfate, sodium dodecylbenzene sulfonate, C₁₄-C₁₆ α-olefin sulfonate, oleoyl methyltaurine, alkyl sulfosuccinate, sodium stearate, alkyl substituted disulfonated diphenyloxide and nonylphenoxy oligo(ethylene glycol) sulfate. Ionic polymers can be used, including polyethyleneimine, polyacrylic acid, carboxymethyl cellulose and the like. Suitable

cationic surfactants include cetyltrimethyl ammonium bromide, N-methyl(4-dodecylpyridinium bromide). Suitable nonionic surfactants include ethoxylated mono-, di- and trialkylphenols (degree of ethoxylation: 3 to 100, alkyl radical: C₄ to C₁₂), ethoxylated fatty alcohols (degree of ethoxylation: 3 to 100, preferably 6 to 50, alkyl radical: C₆ to C₂₀) and alkali metal and ammonium salts of alkylsulfates (alkyl radical: C₈ to C₁₈), of sulfuric half-esters of ethoxylated alkanols (degree of ethoxylation: 1 to 70, in particular 2 to 10, alkyl radical: C₁₀ to C₁₈) and of ethoxylated alkylphenols (degree of ethoxylation: 3 to 100, preferably 6 to 50, alkyl radical: C₄ to C₁₈) and alkali metal and ammonium salts of alkanesulfonic acids (alkyl radical: C₁₀ to C₁₈) and of alkylarylsulfonic acids (alkyl radical: C₉ to C₁₈). Further suitable surfactants, such as sulfosuccinates, are described in Houben-Weyl, Methoden der organischen Chemie, Volume XIV/1, Makromolekulare Stoffe, Georg-Thieme Verlag, Stuttgart, 1961, pages 192 to 208. Alternative surfactants include functional monomers, polymerizable surfactants and water-soluble surface-active polymers, including block copolymers, such as polyethyleneoxide-b-polypropyleneoxide-b-polyethyleneoxide (Pluronic®). Specific examples include polyvinyl alcohols, cellulose derivatives or vinylpyrrolidone-containing copolymers. A detailed description of further suitable protective colloids is given in Houben-Weyl, Methoden der organischen Chemie, Volume XIV/1, Makromolekulare Stoffe, Georg-Thieme-Verlag, Stuttgart, 1961, pages 411 to 420.

Currently commercially available surfactants that are useful in this invention are listed below in Table 1.

Table 1:

Trade Name	Supplier	Contents
Ionics		
Abex VA-50	Rhodia	46%; 1:1 mix of anionic and ethoxylated octyl phenol
Abex 2020	Rhodia	Anionic/non-ionic mix (APE free), 30%
Abex 2030	Rhodia	Anionic/non-ionic mix (APE free), 30%
Abex 18-S	Rhodia	Na Ether Sulfates; APE-free, 35%
Abex 12-S	Rhodia	Na Ether Sulfates; APE-free, 30%
Aerosol OT	Sigma	[(Bis-2-ethylhexyl)sodium sulfosuccinate, C ₂₀ H ₃₇ O ₇ S.Na, M _w 444.6, 10%]
Aerosol 22	Sigma	[(Bis-2-ethylhexyl)sodium sulfosuccinate, C ₂₀ H ₃₇ O ₇ S.Na, M _w 444.6, neat d=1.12]
Calfax DB-45	Pilot Chemical	C ₁₂ (branched) Sodium diphenyloxide disulfonate, 45%
Calfax 16L-35	Pilot Chemical	C ₁₆ (linear) Sodium diphenyloxide disulfonate, 35%
Calimulse L-30	Pilot Chemical	Sodium linear alkyl benzene sulfonate 30%
Calimulse EM-30	Pilot Chemical	Sodium branched dodecyl benzene sulfonate 30%

Trade Name	Supplier	Contents
Calsoft F-90	Pilot Chemical	Sodium linear alkyl benzene sulfonate, solid, 90+%
Dowfax C6L	Dow	Disulfonated diphenyloxide with C ₆ backbone
Dowfax C10L	Dow	Disulfonated diphenyloxide with C ₁₀ backbone
Dowfax 8390	Dow	Disulfonated diphenyloxide with C ₁₆ backbone, 45%
Emulgator 825	BASF	anionic/non-ionic mix
Emulgator 825-S	BASF	anionic/non-ionic mix
Rhodacal A-246/L	Rhodia	sodium alpha C ₁₄ -C ₁₆ olefin sulfonate (38-41%)
Rhodacal DS-4	Rhodia	sodium dodecyl benzene sulfonate 23%
SDS	Aldrich	sodium dodecyl sulfate
SDBS	Aldrich	sodium dodecyl benzene sulfonate 90%
Triton QS-30	Union Carbide	90%, gel like
Triton X-200	Union Carbide	28% aq dispersion
Aphos 3232	ICI	Polyoxyethylene phosphate ester
Aphos 3226	ICI	anionic sfac, phosphoric acid
Aphos 3202	ICI	NonylPE n=6, acid form, 100%
Nonionics		
Abex 2545	Rhodia	
Abex 2535	Rhodia	
Dynol 604	Air Products	Ethoxylated acetylenic diols, 100%
Igepal CO-210	Aldrich	APE (C ₉ H ₁₉ -C ₆ H ₄ -(OCH ₂ CH ₂) ₂ OH) 100%
Igepal CO-520	Aldrich	APE (C ₉ H ₁₉ -C ₆ H ₄ -(OCH ₂ CH ₂) ₅ OH) 100%
Igepal CA-897	Rhodia	APE (octylphenol ethoxylate) 70%, n=40
Igepal CO-897	Rhodia	APE (nonylphenol ethoxylate) 70% n=40
Pluronic F38	BASF	EO-PO-EO block, average M _w 4700 HLB 31
Pluronic F98	BASF	EO-PO-EO block, average M _w 13K, HLB 28
Pluronic P65	BASF	EO-PO-EO block, average M _w 3400 HLB 17
Surfynol 104 PA	Air Products	50% in isopropyl alcohol, 50% 2,4,7,9-tetramethyl-5-decyne-4,7,-diol
Surfynol 104 PG-50	Air Products	50% in propylene glycol, 50% 2,4,7,9-tetramethyl-5-decyne-4,7,-diol
Surfynol DF-58	Air Products	silicone-based
Surfynol 440	Air Products	Surfynol 104 with ethylene oxide chains, more hydrophilic, 100%
Surfynol 465	Air Products	Surfynol 104 with ethylene oxide chains, more hydrophobic, 100%
Triton X-100	Union Carbide	t-octylphenoxy-polyethoxyethanol (n=9.5), 100%
Triton X-405	Union Carbide	t-octylphenoxy-polyethoxyethanol, 70%

[0100] The process of the invention does not necessarily require surfactant. For example, surfactant-free recipes can be used where the sulfate groups on a persulfate initiator impart the latex stability. In this case, relatively large ratios of initiator to monomer are used (e.g., 50:1 to 250:1) and large particles result (e.g., 300-600 nm). The ratios of components (e.g., initiators, surfactants, monomers, and control agents) in the polymerization mixture may be important and can vary widely depending on the particular application. The ratio of monomer to control agent can be used to determine the molecular weight of polymers produced using the controlled heterogeneous free radical polymerization processes of the invention. According to these processes, the

number average molecular weight of the resulting polymers depends linearly on the number of control agents in the polymerization and the mass of monomer.

[0101] In some embodiments, the monomer to initiator ratio may be in the range of from about 10:1 to about 10,000:1, more preferably the range of from about 50:1 to about

5 10,000:1 and most preferably the range of from about 100:1 to about 5000:1. Another ratio that may be controlled is the ratio of equivalents of initiator to control agent, (with the assumption that the amount of initiator is approximately equivalent to the number of radical produced), which is typically in the range of from about 1:0.1 to about 1:10, more preferably the range of from about 1:0.3 to about 1:5 and most preferably the range of

10 from about 1:0.4 to about 1:2. When a redox system is used, it may be present the ratio of initiator to reductant typically in the range of from about 1:0.1 to about 1:4, more preferably the range of from about 1:0.3 to about 1:2 and most preferably the range of from about 1:0.4 to about 1:1.6. The surfactant to monomer ratio may be controlled and is typically in the range of from about 0.0001 to about 2:1, more preferably the range of

15 from about 0.001:1 to about 0.05:1 and most preferably the range of from about 0.001:1 to about 0.02:1 (although for some emulsions there may be no surfactant added at all where other reaction components perform that function). The percent solids may be in the range of from 0.001% to about 90% by volume. In some preferred applications, the novel aqueous polymer emulsions are produced with a solids content of = 40%,

20 advantageously = 50%, by volume, based on the total aqueous polymer emulsion. The useful solids content for other applications is from 0.5 to 75% by volume. The preparation of the novel aqueous polymer emulsions is carried out according to the product by process definition of the subject according to the invention, as stated at the outset, *i.e.*, by the free radical aqueous emulsion polymerization method in the presence

25 of surface active materials and free radical polymerization initiators. The ratio of the aqueous phase to the total amount of the monomers used in both stages is chosen according to the desired solids content of the aqueous polymer emulsion to be prepared.

[0102] The emulsion process can be implemented in a batch, semi-batch or continuous mode. In one embodiment the reaction is operated in such a way as to convert the

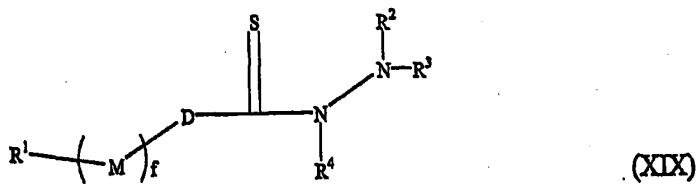
30 control agent into dormant chains early in the process. For example, the consumption of the control agent is substantially completed when the cumulative monomer conversion (defined as the ratio monomer converted at time *t* to the total monomer present in the recipe) is less than about 30%, more specifically less than about 20% and even more

specifically less than about 10%. This can be performed by adjusting polymerization process variables, such as the sequence and feed-rate of addition of monomers, control agents, initiators, etc. For example, in a semi-batch polymerization process where a fraction of the monomer is introduced initially in the reactor and the remaining fraction fed over a period of time, the control agent is preferentially added in totality in the initial charge. In a continuous polymerization process (e.g., using either a recirculation loop or a series of continuously stirred tank reactors), the control agent is preferably fed in the upstream part of the continuous process. A preferred polymerization process is semi-batch, with the totality of the control agent fed to the initial charge and where the feed rate of the monomer stream is adjusted to a "starved feed regime", i.e., where the monomer to polymer ratio is maintained below 0.2, preferably 0.05, until the control agent is totally consumed (as measured by gas or liquid chromatography). Process variables that may coincide to control the monomer to polymer ratio are rate of monomer additions, initiator to monomer ratios, temperature and particle size.

[0103] A free radical source is provided in the polymerization mixture, which can stem from spontaneous free radical generation upon heating or preferably from a free radical initiator. In the latter case the initiator is added to the polymerization mixture at a concentration high enough to for an acceptable polymerization rate (e.g., commercially significant conversion in a certain period of time, such as listed below). Conversely, a too high free radical initiator to control agent ratio will favor unwanted dead polymer formation through radical-radical coupling reaction leading to polymer materials with uncontrolled characteristics. The molar ratio of free radical initiator to control agent for polymerization are typically in the range of from about 2:1 to about 0.02:1.

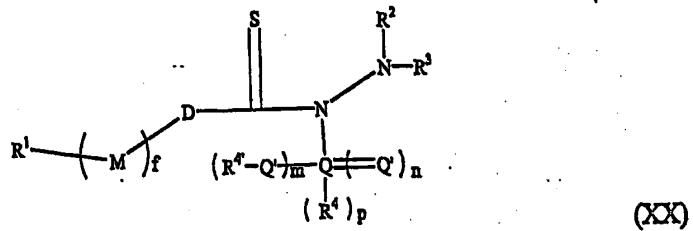
25 Polymers

[0104] The polymers formed with the chain transfer agents of this invention are believed to be grown via a degenerative transfer mechanism. Thus, upon analysis of the obtained polymers, monomers might appear between the R^1-S bond, and any of the above formulas can be rewritten in a polymeric form. For example, the polymers of this invention may be characterized by the general formula:



wherein M is a monomer or mixture of monomers or at least 2 blocks of different monomer (any from the above lists) and f is the degree of polymerization, and D, R¹, R², R³ and R⁴ are as defined above.

5 [0105] For the more specific embodiment, the polymer of this invention, the polymers may be characterized by the general formula:

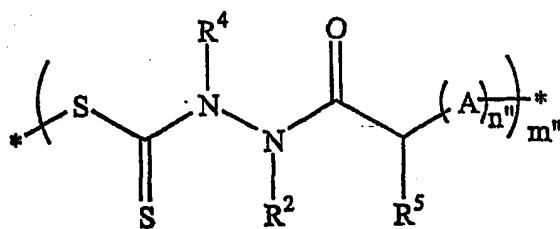


wherein M is a monomer or mixture of monomers or at least 2 blocks of different monomer (any from the above lists) and f is the degree of polymerization, and Q, Q', n, D, R¹, R², R³ and R⁴ are as defined above.

10 [0106] Free radical polymerization of cyclic monomers by ring opening mechanism is known (see, e.g., The Chemistry Of Free Radical Polymerization, G.Moad, D.H.Solomon, Eds. (Pergamon Pub., 1995), p 176 -183). However no commercially viable process has been developed so far. This is due at least in part to the poor

15 reactivity of these monomer compounds (e.g., Ketene acetals) as well as their relative instability to water traces. Moreover, known polymerization mechanisms for ring opening polymerization systems are not known for their living-type kinetics.

[0107] Surprisingly it has been found that the cyclized forms of the multi-functional control agents (such as those described by formulas (XIII) and (XIV)) lead to ring opening reaction under polymerization conditions. The polymer thus formed may be 20 characterized by the general formula:

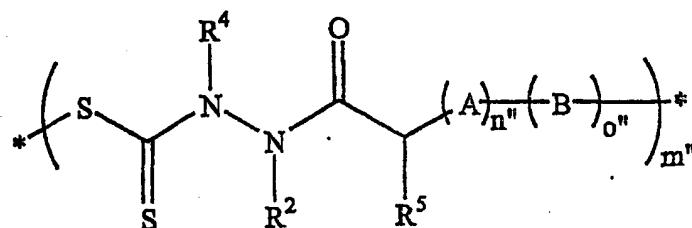


(XXI)

where R^2 , R^4 and R^5 have the same definitions given above and A represents a repeat unit of block of monomer A (with n'' being the degree of polymerization of the block; m'' being the number of repeat units of the block with the attached control agent; and * representing the ends of the polymer). The molecular weight of the polymer formed from monomer A is generally controlled by controlling the monomer to control agent ratio in the polymerization mixture, as discussed above.

[0108] As formula (XXI) shown, the multi-functional control agents of this invention also provide, in some embodiments, for a dithiocarbazate compound (i.e., $N-NC(=S)S$) in the backbone of a carbon-carbon polymer chain, such as usually obtained by free radical polymerization of ethylenic monomers. This is desirable for several applications: for instance, such polymers can be reduced to low molecular weight material by applying external stimuli such as UV, light, heat, biochemical or chemical treatment, which are known to cleave thiocarbonylthio linkage. Such polymers could be used as thermoplastics susceptible to degradation by exposure to sunlight, or by enzymatic digestion since it is known that short polymers chains are readily biodegradable.

[0109] Moreover, multiblock copolymers $(ABx)_y$ can be obtained in a two-step process, by first preparing a first multiblock homopolymer, denoted $(Ax)_y$, where x represents the dithiocarbazate $N-NC(=S)S$ moiety and y represents the number of A or AB blocks and y is 2 or more, and then adding monomer B, in order to get $(ABx)_y$, which may be characterized by the general formula:

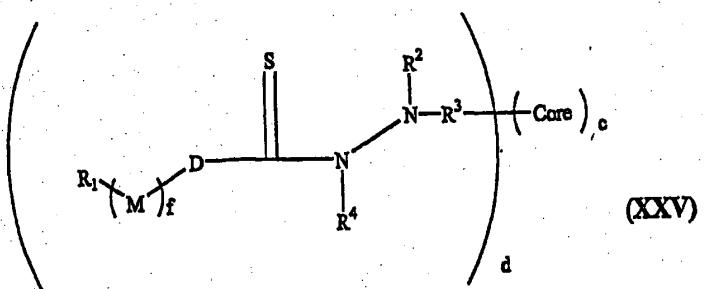
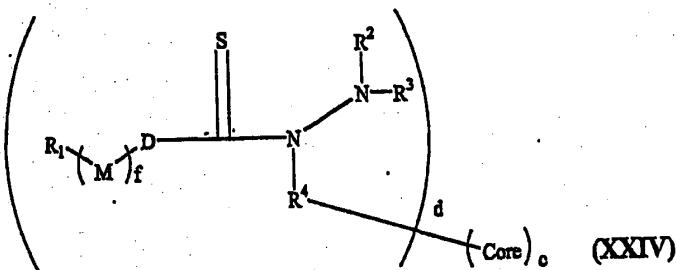
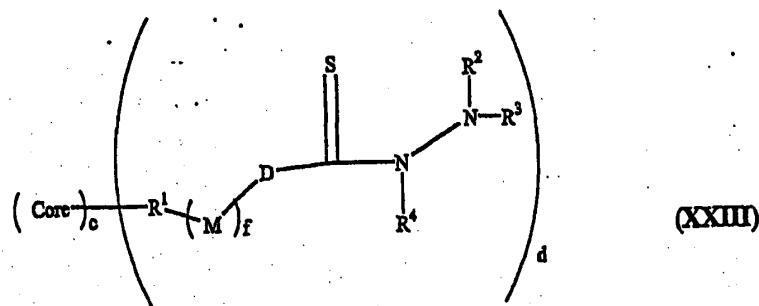


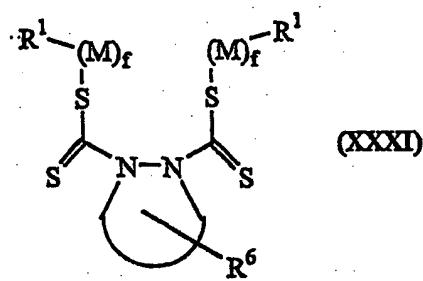
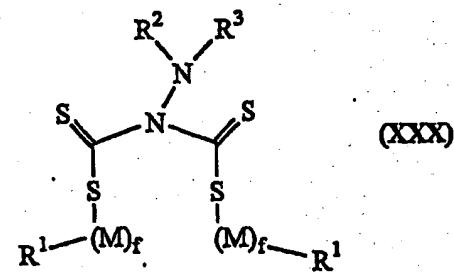
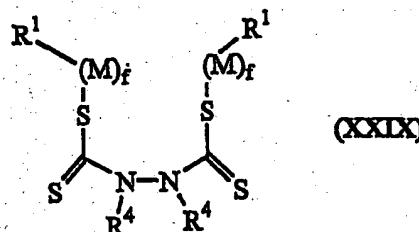
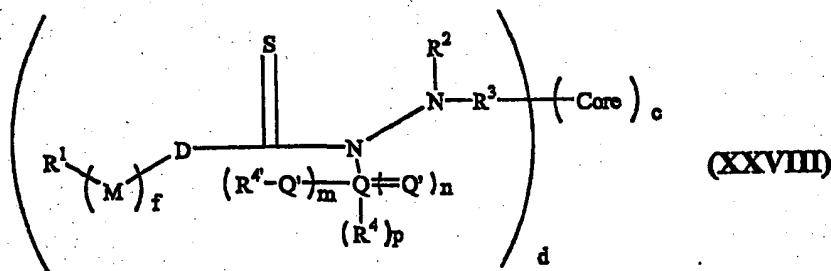
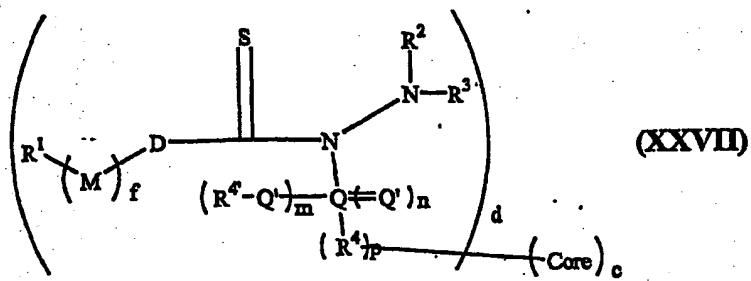
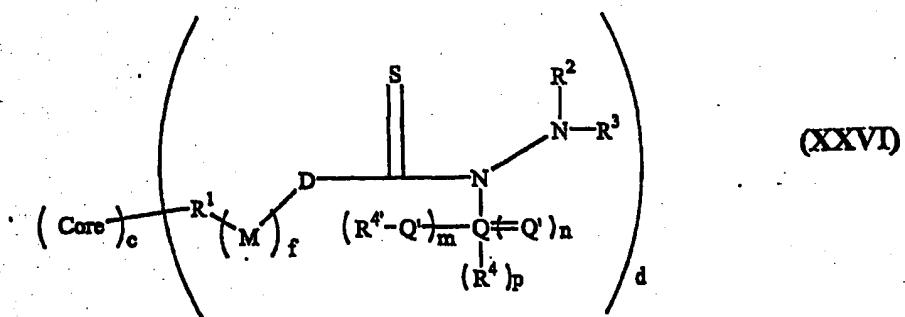
(XXII)

where R^2 , R^4 and R^5 and n'' and m'' have the same definitions given above, A represents a repeat unit of block of monomer A and B represents a repeat unit of block of monomer

B and n " is the degree of polymerization of monomer B. Monomers A and B can be selected from any of the above lists. Copolymers having a similar structure as (AB) $_n$ copolymers are usually prepared by multiple sequential addition of different monomers with the usual pitfalls such as loss of control as long as the number of block increase or 5 contamination of block A with B monomers. This new process alleviates these difficulties.

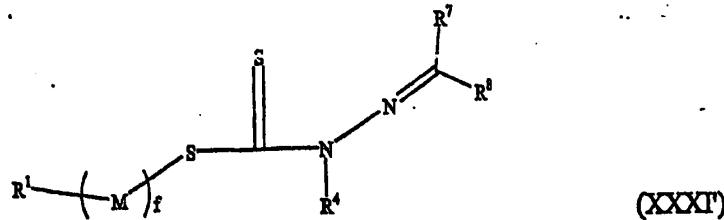
[0110] The formulas for multifunctional control agents can also be written in polymer form, as follows:





wherein each of the variable in formulas (XXIII) to (XXXI) have the above stated meanings.

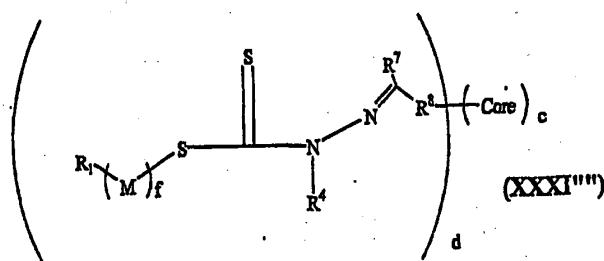
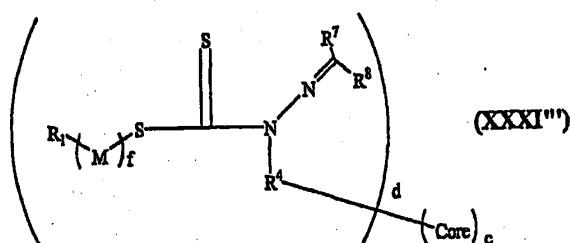
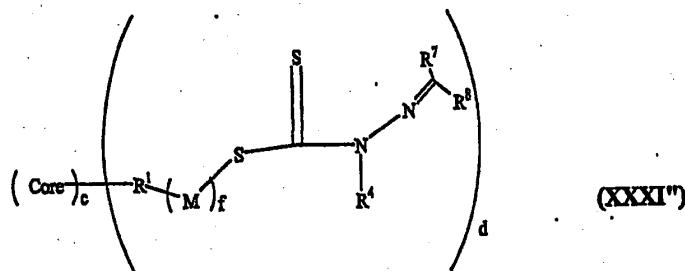
[0111] The polymers of this invention may be characterized by the general formula:



5 wherein M is a monomer or mixture of monomers or at least 2 blocks of different monomer (any from the above lists) and f is the degree of polymerization, and R¹, R⁴, R⁷ and R⁸ are as defined above.

[0112] The formulas for multifunctional control agents in the emulsion embodiment can also be written in polymer form, as follows:

10



wherein each of the variable in formulas (XXXI') to (XXXI''') have the above stated meanings.

[0113] In some embodiments of this invention, it is desirable to make a block copolymer, such as for example with both hydrophobic and hydrophilic monomers, with these monomers being selected from the above lists. In this case, the monomers M in the above formulas will be A and B or more blocks.

5 [0114] As used herein, "block copolymer" refers to a polymer comprising at least two segments of differing composition; having any one of a number of different architectures, where the monomers are not incorporated into the polymer architecture in a solely statistical or uncontrolled manner. Although there may be three, four or more monomers in single block-type polymer architecture, it will still be referred to herein as a block copolymer. In some embodiments, the block copolymer will have an A-B architecture (with "A" and "B" representing the monomers). Other architectures included within the definition of block copolymer include A-B-A, A-B-A-B, A-B-C, A-B-C-A, A-B-C-A-B, A-B-C-B, A-B-A-C (with "C" representing a third monomer), and other combinations that will be obvious to those of skill in the art. Block copolymers can 10 be prepared a number of ways, including sequential addition of monomers or using multi-functional control agents described above. Of course with multi-functional control agents, the control agent may form a linking group between one or more blocks of the copolymers.

15 [0115] In another embodiment, the block copolymers of this invention include one or more blocks of random copolymer together with one or more blocks of single monomers. Thus, a polymer architecture of A-R, A-R-B, A-B-R, A-R-B-R-C, etc. is included herein, where R is a random block of monomers A and B or of monomers B and C. Moreover, the random block can vary in composition or size with respect to the overall block copolymer. In some embodiments, for example, the random block R will account for 20 between 5 and 80 % by weight of the mass of the block copolymer. In other embodiments, the random block R will account for more or less of the mass of the block copolymer, depending on the application. Furthermore, the random block may have a compositional gradient of one monomer to the other (e.g., A:B) that varies across the random block in an algorithmic fashion, with such algorithm being either linear having a 25 desired slope, exponential having a desired exponent (such as a number from 0.1-5) or logarithmic. The random block may be subject to the same kinetic effects, such as composition drift, that would be present in any other radical copolymerization and its 30 composition, and size may be affected by such kinetics, such as Markov kinetics. Any of

the monomers listed elsewhere in this specification may be used in the block copolymers of this invention.

[0116] A "block" within the scope of the block copolymers of this invention typically comprises about 10 or more monomers of a single type (with the random blocks being defined by composition and/or weight percent, as described above). In preferred embodiments, the number of monomers within a single block is about 15 or more, about 20 or more or about 50 or more. However, in an alternative embodiment, the block copolymers of this invention include blocks where a block is defined as two or more monomers that are not represented elsewhere in the copolymer. This definition is intended to encompass adding small amounts of a second monomer at one or both ends of a substantially homopolymeric polymer. In this alternative embodiment, the same copolymer architectures discussed above apply. This definition is therefore intended to include telechelic polymers, which include one or more functional end groups capable of reacting with other molecules. Thus, generally, a telechelic polymer is a block copolymer within the definitions of this invention. The functional groups present at one or both ends of a telechelic polymer may be those known to those of skill in the art, including, for example, hydroxide, aldehyde, carboxylic acid or carboxylate, halogen, amine and the like, which have the ability to associate or form bonds with another molecule. Likewise, the block copolymers of the invention are intended to encompass telechelic polymers containing bifunctional groups, such as allyl-terminated or vinyl-terminated telechelics, sometimes referred to as macromonomers or macromers because of their ability to participate in polymerization reactions through the terminal functional group.

[0117] Combining the above embodiments provides a particularly powerful method of designing block copolymers. For example, a block copolymer may have the architecture F-A-B-F, where F represents functional groups that may be the same or different within a single F-A-B-F structure (which, therefore, may encompass F-A-B-F'). Other block copolymer architectures within the scope of this invention include A-R-B-F and F-A-R-B-F. Other architectures will be apparent to those of skill in the art upon review of this specification – indeed, without wishing to be bound by any particular theory – it is the living nature of the emulsions of this invention that provide the ability to even make these novel block copolymers.

[0118] In one embodiment, block copolymers are assembled by the sequential addition of different monomers or monomer mixtures to living polymerization reactions. In another embodiment, the addition of a pre-assembled functionalized block (such as a telechelic oligomer or polymer) to a living free radical polymerization mixture yields a block copolymer. Ideally, the growth of each block occurs to high conversion.

5 Conversions are determined by size exclusion chromatography (SEC) via integration of polymer to monomer peak. For UV detection, the polymer response factor must be determined for each polymer/monomer polymerization mixture. Typical conversions can be 50% to 100 % for each block. Intermediate conversion can lead to block copolymers with a random copolymer block separating the two or more homopolymer blocks, depending on the relative rates of polymerization and monomer addition. At high conversion, the size of this random block is sufficiently small such that it is less to affect polymer properties such as phase separation, thermal behavior and mechanical modulus. This fact can be intentionally exploited to improve polymerization times for many applications without measurably affecting the performance characteristics of the resulting polymer. This is achieved by intentionally "killing" or terminating the living nature of the polymerization when a desired level of conversion (e.g., >80%) is reached by neutralizing the control agent, for example by introducing acids, bases, oxidizing agents, reducing agents, radical sources, scavengers, etc. In the absence of control agent, the polymerization continues uncontrolled (typically at much higher reaction rates) until the remaining monomer is consumed. Block copolymer can also be created by grafting monomers, monomer mixtures, oligomers or polymers only polymers having multiple available functional groups.

10 [0119] In other embodiments, block copolymers can be prepared by grafting processes, preparation of telechelic polymers, preparation of macromonomers, etc. In these embodiments, at least one polymer segment is derived from a living or controlled process of the invention, while other segments can be derived from any polymerization process, including, for example, controlled or uncontrolled radical polymerization, condensation polymerization, Ziegler-Natta and related processes, Ring-Opening

15 [0120] Metathesis Polymerization, ionic polymerization, surface modification or grafting, or other addition or step-growth processes.

20 [0121] Block copolymers allow the combination of potentially diverse polymer properties (such as hard/soft and/or hydrophilic/hydrophobic (amphiphilic) blocks) into a

single polymer chain. Hard/soft block copolymers combine segments with significantly different glass transition temperatures T_g . A typical hard/soft copolymer pairs a relatively "hard" block (e.g., styrene) with a relatively "soft" block (e.g., butyl acrylate). The resulting materials can possess performance attributes not found in any of the 5 constituent segments. The presence of microphase separation and various phase morphologies in block copolymers is associated with unique performance attributes of many block copolymers. For example, by combining the stiffness or rigidity characteristic of hard materials with the compliance of soft materials, block copolymers may exhibit advantageous properties, such as processability under melt conditions, 10 elasticity, resistance to abrasion and cracking and desired creep characteristics (corresponding to the material's ability to hold its shape under external stresses) depending on morphology, making them appropriate for use as extrudable bulk materials, coatings and separation media. The exact properties of a hard/soft copolymer depend significantly on the difference between the glass transition temperatures of the 15 constituent blocks; accordingly, selection of monomers having glass transition temperatures a particular distance apart can lead to hard/soft block copolymers having particular desired characteristics. Thus, while for one application it may be appropriate to combine blocks having glass transition temperatures that differ by, for example, 20°C, the choice of T_g (and therefore of materials) depends on the application.

20 [0121] Likewise, the amphiphilic block copolymers produced according to the invention display combinations of hydrophobic and hydrophilic properties that make such materials appropriate for use as surfactants or dispersants, scavengers, surface treatments and the like. Different block sizes over all ratios of monomers and molecular weights lead to families of novel compounds, for example thermoplastics, elastomers, adhesives, 25 and polymeric micelles.

[0122] Multi-arm or star polymers can be generated using initiators capable of initiating multiple free radical polymerizations under the controlled conditions of the invention. Such initiators include, for example polyfunctional chain transfer agents, discussed above. Following initiation, the growth of each arm is controlled by the same living 30 kinetics described for linear polymers, making it possible to assemble star polymers whose arms include individual homopolymers as well as di, tri or higher order block copolymers. Alternatively, multi-arm polymers are formed by growing end-functionalized oligomers or polymers followed by the addition of a cross-linking

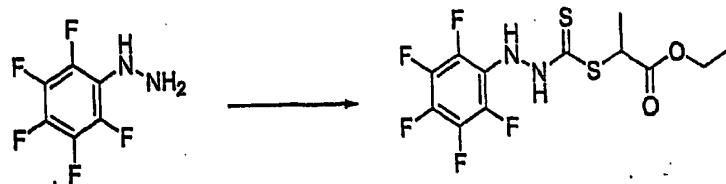
monomer such as ethylene glycol diacrylate, divinyl benzene, methylene bisacrylamide, trimetylol propane triacrylate, etc. The small hydrodynamic volume of star polymers produced according to these methods provides properties such as low viscosity, high M_w , and high functionality useful in applications such as rheology control, thermosets, 5 and separation media. Similarly, the inclusion of branched or multiple ethylenically unsaturated monomers enables the preparation of graft polymers, again exhibiting the living kinetics characteristic of this invention. The existence of a block copolymer according to this invention is determined by methods known to those of skill in the art, including nuclear magnetic resonance (NMR), measured increase of molecular weight 10 upon addition of a second monomer to chain-extend a living polymerization of a first monomer, microphase separation (e.g., long range order, microscopy and/or birefringence measurements), mechanical property measurements, (e.g., elasticity of hard/soft block copolymers), thermal analysis and chromatography (e.g., absence of homopolymer).

15

EXAMPLES

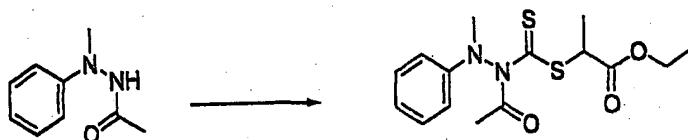
[0123] **General:** Syntheses of control agents were carried out under a nitrogen or argon atmosphere. Other chemicals were purchased from commercial sources and used 20 as received, except for monomers, which were filtered through a short column of basic aluminum oxide to remove any inhibitor and degassed by applying vacuum. All polymerization mixtures were prepared in a glove box under a nitrogen or argon atmosphere and sealed, and polymerization was conducted at 60°C or 70°C. Size Exclusion Chromatography was performed using an automated rapid GPC system for the 25 primary screening (see WO 99/51980, incorporated herein by reference) and using automated conventional GPC system for secondary screening. In the current setup N,N-dimethylformamide containing 0.1 % of trifluoroacetic acid was used as an eluent for the rapid GPC system whereas THF for the conventional system and polystyrene-based columns. All of the molecular weight results obtained are relative to linear polystyrene 30 standards. NMR was carried out using a Bruker spectrometer (300 MHz) with $CDCl_3$ (chloroform-*d*) as solvent.

EXAMPLE 1:

**A'-1****A-1**

[0124] A 50 mL round-bottomed flask equipped with a magnetic stir bar and maintained under a nitrogen atmosphere was charged with hydrazine A'-1 (4.0 g, 20 mmol), sodium hydroxide (0.8 g, 20 mmol), and ethanol (20 mL). The reaction mixture was kept cold in an ice/water bath. To the resulting solution, carbon disulfide (1.21 mL, 20 mmol) was added dropwise. The mixture was stirred for an additional one hour after the addition was finished. Ethyl 2-bromopropionate (2.6 mL, 20 mmol) was then added to the reaction mixture at 0 °C. After the reaction was completed, as monitored by thin layer chromatography (TLC), the reaction mixture was poured into 80 mL of water and followed by extraction with ethyl acetate (2×80 mL). The organic layer was further washed with water (2×80 mL) and dried over MgSO₄. The solvent was removed under reduced pressure and the product was further purified by flash chromatograph. The desired control agent A-1 was obtained in 72% yield (5.4 g).

15 **EXAMPLE 2:**

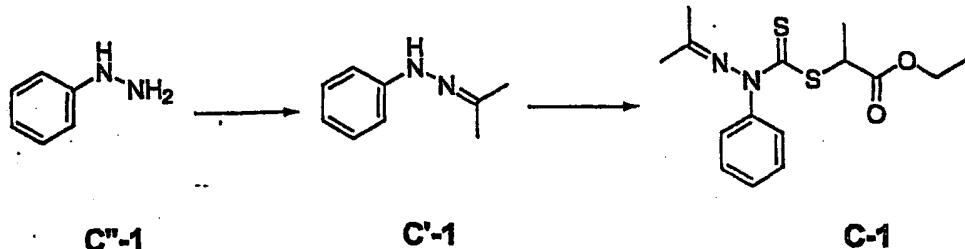
**B'-1****B-1**

[0125] A 50 mL round-bottomed flask equipped with a magnetic stir bar and maintained under a nitrogen atmosphere was charged with hydrazine B'-1 (1.6 g, 10 mmol), sodium hydroxide (0.4 g, 10 mmol), and DMSO (20 mL). The reaction mixture was kept cold in an ice/water bath. To the resulting solution, carbon disulfide (0.6 mL, 10 mmol) was added dropwise. The mixture was stirred for an additional one hour after the addition was finished. Ethyl 2-bromopropionate (1.81 g, 1.3 mL) was then added to the reaction mixture at 0 °C. After the reaction was completed, as monitored by TLC, the reaction mixture was poured into 80 mL of water and followed by extraction with ethyl ether

(2×80 mL). The organic layer was further washed with water (2×80 mL) and dried over MgSO₄. The solvent was removed under reduced pressure and the product was further purified by flash chromatograph. The desired control agent B-1 was obtained in 67% yield (1.6 g).

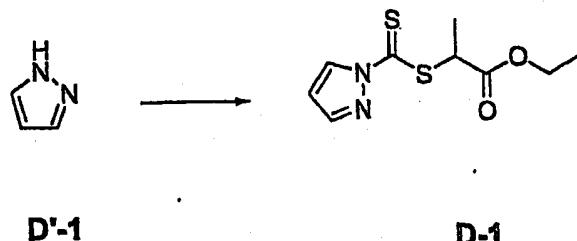
5

EXAMPLE 3:



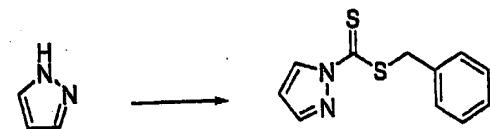
[0126] A 100 mL round-bottomed flask was charged with hydrazine C''-1 (3 mL, 30 mmol), and acetone (20 mL) at ambient temperature. The excess of acetone was removed under reduced pressure to give a quantitative yield of hydrazone C'-1. The flask then equipped with a magnetic stir bar and maintained under a nitrogen atmosphere was charged with sodium hydroxide (1.2 g, 30 mmol), and dimethylsulfoxide (DMSO) (60 mL) at ambient temperature. The reaction mixture was kept in a water bath. To the resulting solution, carbon disulfide (1.8 mL, 30 mmol) was added dropwise. The mixture was stirred for an additional one hour after the addition was finished. Ethyl 2-bromopropionate (3.9 mL, 30 mmol) was then added to the reaction mixture dropwise. After the reaction was completed, as monitored by TLC, the reaction mixture was poured into 120 mL of water and followed by extraction with ethyl acetate (2×80 mL). The organic layer was further washed with water (2×80 mL) and dried over MgSO₄. The solvent was removed under reduced pressure and the product was further purified by flash chromatograph. The desired control agent C-1 was obtained in 65% yield (6.3 g).

EXAMPLE 4:



[0127] A 100 mL round-bottomed flask equipped with a magnetic stir bar and maintained under a nitrogen atmosphere was charged with pyrazole D'-1 (1.36g, 20 mmol), sodium hydroxide (0.8 g, 20 mmol), and DMSO (40 mL). The reaction mixture was kept in an ice/water bath. To the resulting solution, carbon disulfide (1.2 mL, 20 mmol) was added dropwise. The mixture was stirred for an additional one hour after the addition was finished. Ethyl 2-bromopropionate (2.6 mL, 20 mmol) was then added to the reaction mixture dropwise. After the reaction was completed, as monitored by TLC, the reaction mixture was poured into 80 mL of water and followed by extraction with ethyl acetate (2×80 mL). The organic layer was further washed with water (2×80 mL) and dried over MgSO₄. The solvent was removed under reduced pressure and the product was further purified by flash chromatograph. The desired control agent D-1 was obtained in 85% yield (4.15g).

EXAMPLE 5:

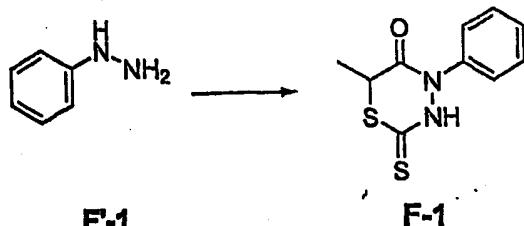


15

E'-1

E-1

[0128] A 100 mL round-bottomed flask equipped with a magnetic stir bar and maintained under a nitrogen atmosphere was charged with pyrazole E'-1 (1.36g, 20 mmol), sodium hydroxide (0.8 g, 20 mmol), and DMSO (40 mL). The reaction mixture was kept in an ice/water bath. To the resulting solution, carbon disulfide (1.2 mL, 20 mmol) was added dropwise. The mixture was stirred for an additional one hour after the addition was finished. Benzyl bromide (2.38 mL, 20 mmol) was then added to the reaction mixture dropwise. After the reaction was completed, monitored by TLC, the reaction mixture was poured into 80 mL of water and followed by extraction with ethyl acetate (2×80 mL). The organic layer was further washed with water (2×80 mL) and dried over MgSO₄. The solvent was removed under reduced pressure and the product was further purified by flash chromatograph. The desired control agent E-1 was obtained in 91% yield (4.3g).

EXAMPLE 6:

[0129] A 100 mL round-bottomed flask equipped with a magnetic stir bar and maintained under a nitrogen atmosphere was charged with hydrazine F'-1 (6 mL, 30 mmol), sodium hydroxide (1.2 g, 30 mmol), and DMSO (60 mL). The reaction mixture was kept in an ice/water bath. To the resulting solution, carbon disulfide (1.8 mL, 30 mmol) was added dropwise. The mixture was stirred for an additional one hour after the addition was finished. Ethyl 2-bromopropionate (3.9 mL, 30 mmol) was then added to the reaction mixture dropwise. After the reaction was completed, as monitored by TLC, the reaction mixture was poured into 120 mL of water and followed by extraction with ethyl acetate (2×80 mL). The organic layer was further washed with water (2×80 mL) and dried over MgSO₄. The solvent was removed under reduced pressure. The crude material was purified by silica gel column chromatography. The desired control agent F-1 was obtained in 55% yield (3.93 g).

EXAMPLES 7-15:

[0130] These examples demonstrate polymerization of various monomers using control agents of this invention, specifically control agents A-1, B-1, C-2 and F-1, whose synthesis is described above. Each of the polymerizations was carried out in the same general way, which is that a 0.6M stock solution of each control agent in THF was first prepared. For each polymerization a single monomer was used in the amount of 3 mmol. 2,2'-azobis(2-methylpropionitrile) (AIBN) was the initiator used in each polymerization in a quantity of 10 mole % relative to the control agent. The control agent in each polymerization was 0.5 mole % relative to the amount of monomer. The polymerization mixture of each reaction was created by automated dispensing of reaction components at room temperature into a glass vial, which was then sealed. Each polymerization reaction was

carried out at 60°C for a time of 1 hour, 4 hours, 12 hours and 16 hours; thus, for each example, the polymerization was carried out four times, once for each time period. The monomers used were styrene (Sty), vinyl acetate (VA), and methyl acrylate (MA), each of which was used in neat form and prepared as discussed at the beginning of the example section. The results of these polymerizations are reported in Table 2, below.

[0131] A series of control experiments was also carried out, where the same polymerization mixtures were created, but no control agent was added. The results of those control experiments are not reported in detail because gels or very high molecular weight polymers were obtained.

Table 2:

Example	Control Agent	Monomer	Reaction Time (hrs)	M _n	M _w /M _n
7	A-1	Sty	1	38900	1.57
			4	35700	1.54
			12	36600	1.57
			16	33700	1.61
8	A-1	VA	1	N/A	N/A
			4	9500	1.14
			12	9300	1.14
			16	10200	1.14
9	A-1	MA	1	65000	1.37
			4	71300	1.32
			12	73000	1.32
			16	64700	1.37
10	B-1	Sty	1	N/A	N/A
			4	5300	1.09
			12	5600	1.09
			16	6500	1.12
11	B-1	MA	1	N/A	N/A
			4	N/A	N/A
			12	8300	1.16
			16	12000	1.17
12	C-1	Sty	1	97300	1.12
			4	55600	1.47
			12	58300	1.5
			16	51500	1.58
13	C-1	MA	1	39800	1.31
			4	47700	1.32
			12	39900	1.36
			16	44400	1.34

Example	Control Agent	Monomer	Reaction Time (hrs)	M _n	M _w /M _n
14	F-1	Sty	1	N/A	N/A
			4	68500	1.35
			12	70700	1.38
			16	54600	1.51
15	F-1	MA	1	273800	1.26
			4	N/A	N/A
			12	263400	1.45
			16	218100	1.44

EXAMPLE 16:

[0132] This example shows butyl acrylate homopolymerization in the presence of the control agent B-1 (which was prepared as above) and in the absence of control agent.

5 [0133] Freshly prepared n-butyl acrylate (5727 uL) and CTA-3 (68 mg) in three reaction vessels were added with 50 uL, 150 uL, and 300 uL of AIBN stock solution (32.8mg/mL in toluene), respectively. In addition, a blank reaction with no control agent was prepared with 50 uL of AIBN stock solution. The polymerizations were carried out at 60 °C for 15 hours in glass vessels that were sealed.

10 [0134] The results are reported in Table 3 and conventional GPC was performed on the samples:

Table 3:

Entry	AIBN (mole% to B-1)	Mn	Mw/Mn	Conv. (%)
1	10	2500	1.60	24
2	30	9400	1.53	50
3	60	14200	1.51	72
4	0.05 mole% of monomer	Crosslinked material		

EXAMPLE 17:

5 [0135] Butyl acrylate and Styrene homopolymerization in the presence of the control agent E-1, as shown above.

[0136] A stock solution mixture of freshly prepared n-butyl acrylate (5727 uL), control agent E-1 (46.8 mg), and AIBN solution in a concentration of 32.8mg/mL in toluene (50 uL) was split into 5 glass 4 mL reaction vessels. Another stock solution mixture of freshly prepared Styrene (4577 uL), control agent E-1 (46.8 mg), and AIBN solution in a concentration of 32.8mg/mL in toluene (50 uL) was also split into 5 glass 4 mL reaction vessels. The polymerizations were carried out at 60 °C and 70 °C for 1 to 22 hours.

10 [0137] The results are reported in Table 4 and conventional GPC was performed on the samples:

15

Table 4:

Entry	Monomer	Temp. (°C)	Time (h)	Mn	Mw/Mn	Conv. (%)
1	n-butyl acrylate	60	2	15700	1.12	70
2	n-butyl acrylate	60	4	18000	1.12	86
3	n-butyl acrylate	60	15	19600	1.14	94
4	n-butyl acrylate	70	1	17400	1.16	85
5	n-butyl acrylate	70	15	20600	1.19	97
6	Styrene	60	4	2900	1.47	11
7	Styrene	60	15	5000	1.37	32
8	Styrene	60	22	6900	1.24	47

Entry	Monomer	Temp. (°C)	Time (h)	Mn	Mw/Mn	Conv. (%)
9	Styrene	70	4	4300	1.40	19
10	Styrene	70	22	6700	1.28	41

Example 18:

[0138] 195 emulsion polymerization experiments were preformed in connection with this example. The polymerizations were performed in glass reactors sealed with septums at the top. Reagents were added via pipette or liquid handling robot. The semi-continuous polymerization process generally involves periodic addition of monomer and other reagents, by depositing about 3-15 μ l of monomer, initiator and surfactant at intervals of about 4-8 minutes, for a total of about 1-2 mL added to each reactor over the course of about 4-5 hours.

[0139] Size Exclusion Chromatography was performed using an automated gel permeation chromatography system with THF as the eluent and polystyrene-based columns, as described in U.S. Patent No. 6,260,407, which is incorporated herein by reference. All of the molecular weight and polydispersity index (PDI) results obtained are relative to linear polystyrene standards. Monomer consumptions were determined by using an automated HP 5800 gas chromatography system (available from Hewlett-Packard). Latex particle sizes were measured by using a parallel dynamic light scattering device, such as that described in U.S. Patent Application No. 09/689,553, filed October 11, 2000, which is incorporated herein by reference. Solid content conversion was based on physically weighting samples using a Bodhan Balance AutomatorTM (available from Mettler-Toledo, Inc., Vernon Hills, IL).

[0140] These examples demonstrate polymerization of *n*-butyl acrylate in emulsion using the control agent C-1, whose synthesis is described above. Each of the polymerizations was carried out in the same general way, a semi-continuous process. Portions of monomer, initiator, and surfactant and other ingredients including water, stabilizing monomer, and sodium bicarbonate were charged initially in the reaction vessel at ambient temperature. The mixture was then brought to the reaction temperature 80 °C in 5 minutes. The rest of monomer in neat and the rest of initiator and surfactant as an aqueous solution were semi-

continuously added, started when reaction reached the reaction temperature, into reaction vessel over a course of 4 hours and 5 hours respectively. After the last addition was finished, each reaction was allowed to further proceed for an additional two hours. For each polymerization a total mass of 3g was carried out.

5 The monomer is in a 33.3 wt% concentration. Sodium persulfate was the initiator used in each polymerization. Surfactants used were sodium dodecyl sulfate (SDS), sodium dodecylbenzenesulfonate (SDBS), a commercial formulation Rhodacal A-246/L. Sodium bicarbonate was used as a buffering agent. Two types of stabilizing monomer including methallyl sulfonate (MS) and acrylic acid (AA) were investigated. The control agent in each polymerization was 0.5 mole % relative to the amount of monomer for a targeted molecular weight of 280,000 g/mol at complete monomer conversion. Automated dispensing of reaction components created the polymerization mixture of each reaction. The detail stoichiometry is reported in Table 5 and the results of these polymerizations are reported in Table 6, below, using the analytical methods described above.

10

15 [0141] A series of control experiments was also carried out, where the same polymerization mixtures were created, but no control agent was added. The results of those control experiments are not reported in detail; in general stable latex with gels or very high molecular weight polymers were obtained.

20

Table 5: Process variables (The numbers are wt% relative to the total monomer)

Entry	Monomer Initial charge/conti nuous addition	Initiator Initial charge/conti nuous addition	Surfactant Type	Surfactant Initial charge/conti nuous addition	NaHCO ₃	Stabilizer type (amount)
2	5/95	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
3	10/90	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
4	15/85	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
5	20/80	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
6	25/75	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
7	30/70	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
8	5/95	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
9	10/90	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
10	15/85	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
11	20/80	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)

Entry	Monomer Initial charge/conti nuous addition	Initiator Initial charge/conti nuous addition	Surfactant Type	Surfactant Initial charge/conti nuous addition	NaHCO ₃	Stabilizer type (amount)
12	25/75	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
13	30/70	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
14	5/95	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
15	10/90	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
16	15/85	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
17	20/80	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
18	25/75	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
19	30/70	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
20	5/95	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
21	10/90	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
22	15/85	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
23	20/80	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
24	25/75	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
25	30/70	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
26	5/95	0.05/0.2	SDS	0.5/1.0	0.30	MS(0)
27	10/90	0.05/0.2	SDS	0.5/1.0	0.30	MS(0)
28	15/85	0.05/0.2	SDS	0.5/1.0	0.30	MS(0)
29	5/95	0.06/0.19	SDS	0.6/0.9	0.30	MS(0)
30	10/90	0.06/0.19	SDS	0.6/0.9	0.30	MS(0)
31	15/85	0.06/0.19	SDS	0.6/0.9	0.30	MS(0)
32	5/95	0.05/0.2	SDS	0.5/1.0	0.30	MS(0.5)
33	10/90	0.05/0.2	SDS	0.5/1.0	0.30	MS(0.5)
34	15/85	0.05/0.2	SDS	0.5/1.0	0.30	MS(0.5)
35	5/95	0.06/0.19	SDS	0.6/0.9	0.30	MS(0.5)
36	10/90	0.06/0.19	SDS	0.6/0.9	0.30	MS(0.5)
37	15/85	0.06/0.19	SDS	0.6/0.9	0.30	MS(0.5)
38	5/95	0.05/0.2	SDS	0.5/1.0	0.30	MS(1.0)
39	10/90	0.05/0.2	SDS	0.5/1.0	0.30	MS(1.0)
40	15/85	0.05/0.2	SDS	0.5/1.0	0.30	MS(1.0)
41	5/95	0.06/0.19	SDS	0.6/0.9	0.30	MS(1.0)
42	10/90	0.06/0.19	SDS	0.6/0.9	0.30	MS(1.0)
43	15/85	0.06/0.19	SDS	0.6/0.9	0.30	MS(1.0)
44	5/95	0.05/0.2	SDS	0.5/1.0	0.30	MS(1.5)
45	10/90	0.05/0.2	SDS	0.5/1.0	0.30	MS(1.5)
46	15/85	0.05/0.2	SDS	0.5/1.0	0.30	MS(1.5)

Entry	Monomer Initial charge/conti nuous addition	Initiator Initial charge/conti nuous addition	Surfactant Type	Surfactant Initial charge/conti nuous addition	NaHCO ₃	Stabilizer type (amount)
47	5/95	0.06/0.19	SDS	0.6/0.9	0.30	MS(1.5)
48	10/90	0.06/0.19	SDS	0.6/0.9	0.30	MS(1.5)
49	15/85	0.06/0.19	SDS	0.6/0.9	0.30	MS(1.5)
50	5/95	0.05/0.2	SDS	0.5/1.0	0.30	AA(0)
51	10/90	0.05/0.2	SDS	0.5/1.0	0.30	AA(0)
52	15/85	0.05/0.2	SDS	0.5/1.0	0.30	AA(0)
53	5/95	0.06/0.19	SDS	0.6/0.9	0.30	AA(0)
54	10/90	0.06/0.19	SDS	0.6/0.9	0.30	AA(0)
55	15/85	0.06/0.19	SDS	0.6/0.9	0.30	AA(0)
56	5/95	0.05/0.2	SDS	0.5/1.0	0.30	AA(0.5)
57	10/90	0.05/0.2	SDS	0.5/1.0	0.30	AA(0.5)
58	15/85	0.05/0.2	SDS	0.5/1.0	0.30	AA(0.5)
59	5/95	0.06/0.19	SDS	0.6/0.9	0.30	AA(0.5)
60	10/90	0.06/0.19	SDS	0.6/0.9	0.30	AA(0.5)
61	15/85	0.06/0.19	SDS	0.6/0.9	0.30	AA(0.5)
62	5/95	0.05/0.2	SDS	0.5/1.0	0.30	AA(1.0)
63	10/90	0.05/0.2	SDS	0.5/1.0	0.30	AA(1.0)
64	15/85	0.05/0.2	SDS	0.5/1.0	0.30	AA(1.0)
65	5/95	0.06/0.19	SDS	0.6/0.9	0.30	AA(1.0)
66	10/90	0.06/0.19	SDS	0.6/0.9	0.30	AA(1.0)
67	15/85	0.06/0.19	SDS	0.6/0.9	0.30	AA(1.0)
68	5/95	0.05/0.2	SDS	0.5/1.0	0.30	AA(1.5)
69	10/90	0.05/0.2	SDS	0.5/1.0	0.30	AA(1.5)
70	15/85	0.05/0.2	SDS	0.5/1.0	0.30	AA(1.5)
71	5/95	0.06/0.19	SDS	0.6/0.9	0.30	AA(1.5)
72	10/90	0.06/0.19	SDS	0.6/0.9	0.30	AA(1.5)
73	15/85	0.06/0.19	SDS	0.6/0.9	0.30	AA(1.5)
74	5/95	0.19/0.31	SDS	1.5/1.0	0	MS (0)
75	5/95	0.19/0.31	SDS	1.5/1.0	0	MS (0.5)
76	5/95	0.19/0.31	SDS	1.5/1.0	0	MS (1.0)
77	5/95	0.19/0.31	SDS	1.5/1.0	0.35	MS (0)
78	5/95	0.19/0.31	SDS	1.5/1.0	0.35	MS (0.5)
79	5/95	0.19/0.31	SDS	1.5/1.0	0.35	MS (1.0)
80	10/90	0.19/0.31	SDS	1.5/1.0	0	MS (0)
81	10/90	0.19/0.31	SDS	1.5/1.0	0	MS (0.5)

Entry	Monomer Initial charge/conti nuous addition	Initiator Initial charge/conti nuous addition	Surfactant Type	Surfactant Initial charge/conti nuous addition	NaHCO ₃	Stabilizer type (amount)
82	10/90	0.19/0.31	SDS	1.5/1.0	0	MS (1.0)
83	10/90	0.19/0.31	SDS	1.5/1.0	0.35	MS (0)
84	10/90	0.19/0.31	SDS	1.5/1.0	0.35	MS (0.5)
85	10/90	0.19/0.31	SDS	1.5/1.0	0.35	MS (1.0)
86	15/85	0.19/0.31	SDS	1.5/1.0	0	MS (0)
87	15/85	0.19/0.31	SDS	1.5/1.0	0	MS (0.5)
88	15/85	0.19/0.31	SDS	1.5/1.0	0	MS (1.0)
89	15/85	0.19/0.31	SDS	1.5/1.0	0.35	MS (0)
90	15/85	0.19/0.31	SDS	1.5/1.0	0.35	MS (0.5)
91	15/85	0.19/0.31	SDS	1.5/1.0	0.35	MS (1.0)
92	20/80	0.19/0.31	SDS	1.5/1.0	0	MS (0)
93	20/80	0.19/0.31	SDS	1.5/1.0	0	MS (0.5)
94	20/80	0.19/0.31	SDS	1.5/1.0	0	MS (1.0)
95	20/80	0.19/0.31	SDS	1.5/1.0	0.35	MS (0)
96	20/80	0.19/0.31	SDS	1.5/1.0	0.35	MS (0.5)
97	20/80	0.19/0.31	SDS	1.5/1.0	0.35	MS (1.0)
98	5/95	0.19/0.31	SDS	1.5/1.0	0	AA (0)
99	5/95	0.19/0.31	SDS	1.5/1.0	0	AA (0.5)
100	5/95	0.19/0.31	SDS	1.5/1.0	0	AA (1.0)
101	5/95	0.19/0.31	SDS	1.5/1.0	0.35	AA (0)
102	5/95	0.19/0.31	SDS	1.5/1.0	0.35	AA (0.5)
103	5/95	0.19/0.31	SDS	1.5/1.0	0.35	AA (1.0)
104	10/90	0.19/0.31	SDS	1.5/1.0	0	AA (0)
105	10/90	0.19/0.31	SDS	1.5/1.0	0	AA (0.5)
106	10/90	0.19/0.31	SDS	1.5/1.0	0	AA (1.0)
107	10/90	0.19/0.31	SDS	1.5/1.0	0.35	AA (0)
108	10/90	0.19/0.31	SDS	1.5/1.0	0.35	AA (0.5)
109	10/90	0.19/0.31	SDS	1.5/1.0	0.35	AA (1.0)
110	15/85	0.19/0.31	SDS	1.5/1.0	0	AA (0)
111	15/85	0.19/0.31	SDS	1.5/1.0	0	AA (0.5)
112	15/85	0.19/0.31	SDS	1.5/1.0	0	AA (1.0)
113	15/85	0.19/0.31	SDS	1.5/1.0	0.35	AA (0)
114	15/85	0.19/0.31	SDS	1.5/1.0	0.35	AA (0.5)
115	15/85	0.19/0.31	SDS	1.5/1.0	0.35	AA (1.0)
116	20/80	0.19/0.31	SDS	1.5/1.0	0	AA (0)

Entry	Monomer Initial charge/conti nuous addition	Initiator Initial charge/conti nuous addition	Surfactant Type	Surfactant Initial charge/conti nuous addition	NaHCO ₃	Stabilizer type (amount)
117	20/80	0.19/0.31	SDS	1.5/1.0	0	AA (0.5)
118	20/80	0.19/0.31	SDS	1.5/1.0	0	AA (1.0)
119	20/80	0.19/0.31	SDS	1.5/1.0	0.35	AA (0)
120	20/80	0.19/0.31	SDS	1.5/1.0	0.35	AA (0.5)
121	20/80	0.19/0.31	SDS	1.5/1.0	0.35	AA (1.0)
122	5/95	0.1/0.4	SDBS	0.5/2.0	0.35	MS (0)
123	10/90	0.1/0.4	SDBS	0.5/2.0	0.35	MS (0)
124	15/85	0.1/0.4	SDBS	0.5/2.0	0.35	MS (0)
125	5/95	0.1/0.4	SDBS	0.5/2.0	0.35	MS (0.5)
126	10/90	0.1/0.4	SDBS	0.5/2.0	0.35	MS (0.5)
127	15/85	0.1/0.4	SDBS	0.5/2.0	0.35	MS (0.5)
128	5/95	0.12/0.38	SDBS	0.6/1.9	0.35	MS (0)
129	10/90	0.12/0.38	SDBS	0.6/1.9	0.35	MS (0)
130	15/85	0.12/0.38	SDBS	0.6/1.9	0.35	MS (0)
131	5/95	0.12/0.38	SDBS	0.6/1.9	0.35	MS (0.5)
132	10/90	0.12/0.38	SDBS	0.6/1.9	0.35	MS (0.5)
133	15/85	0.12/0.38	SDBS	0.6/1.9	0.35	MS (0.5)
134	5/95	0.14/0.36	SDBS	0.7/1.8	0.35	MS (0)
135	10/90	0.14/0.36	SDBS	0.7/1.8	0.35	MS (0)
136	15/85	0.14/0.36	SDBS	0.7/1.8	0.35	MS (0)
137	5/95	0.14/0.36	SDBS	0.7/1.8	0.35	MS (0.5)
138	10/90	0.14/0.36	SDBS	0.7/1.8	0.35	MS (0.5)
139	15/85	0.14/0.36	SDBS	0.7/1.8	0.35	MS (0.5)
140	5/95	0.16/0.34	SDBS	0.8/1.7	0.35	MS (0)
141	10/90	0.16/0.34	SDBS	0.8/1.7	0.35	MS (0)
142	15/85	0.16/0.34	SDBS	0.8/1.7	0.35	MS (0)
143	5/95	0.16/0.34	SDBS	0.8/1.7	0.35	MS (0.5)
144	10/90	0.16/0.34	SDBS	0.8/1.7	0.35	MS (0.5)
145	15/85	0.16/0.34	SDBS	0.8/1.7	0.35	MS (0.5)
146	5/95	0.1/0.4	Rhodacal A-246/L	0.5/2.0	0.35	MS (0)
147	10/90	0.1/0.4	Rhodacal A-246/L	0.5/2.0	0.35	MS (0)
148	15/85	0.1/0.4	Rhodacal A-246/L	0.5/2.0	0.35	MS (0)
149	5/95	0.1/0.4	Rhodacal A-246/L	0.5/2.0	0.35	MS (0.5)

Entry	Monomer Initial charge/conti nuous addition	Initiator Initial charge/conti nuous addition	Surfactant Type	Surfactant Initial charge/conti nuous addition	NaHCO ₃	Stabilizer type (amount)
150	10/90	0.1/0.4	Rhodacal A-246/L	0.5/2.0	0.35	MS (0.5)
151	15/85	0.1/0.4	Rhodacal A-246/L	0.5/2.0	0.35	MS (0.5)
152	5/95	0.12/0.38	Rhodacal A-246/L	0.6/1.9	0.35	MS (0)
153	10/90	0.12/0.38	Rhodacal A-246/L	0.6/1.9	0.35	MS (0)
154	15/85	0.12/0.38	Rhodacal A-246/L	0.6/1.9	0.35	MS (0)
155	5/95	0.12/0.38	Rhodacal A-246/L	0.6/1.9	0.35	MS (0.5)
156	10/90	0.12/0.38	Rhodacal A-246/L	0.6/1.9	0.35	MS (0.5)
157	15/85	0.12/0.38	Rhodacal A-246/L	0.6/1.9	0.35	MS (0.5)
158	5/95	0.14/0.36	Rhodacal A-246/L	0.7/1.8	0.35	MS (0)
159	10/90	0.14/0.36	Rhodacal A-246/L	0.7/1.8	0.35	MS (0)
160	15/85	0.14/0.36	Rhodacal A-246/L	0.7/1.8	0.35	MS (0)
161	5/95	0.14/0.36	Rhodacal A-246/L	0.7/1.8	0.35	MS (0.5)
162	10/90	0.14/0.36	Rhodacal A-246/L	0.7/1.8	0.35	MS (0.5)
163	15/85	0.14/0.36	Rhodacal A-246/L	0.7/1.8	0.35	MS (0.5)
164	5/95	0.16/0.34	Rhodacal A-246/L	0.8/1.7	0.35	MS (0)
165	10/90	0.16/0.34	Rhodacal A-246/L	0.8/1.7	0.35	MS (0)
166	15/85	0.16/0.34	Rhodacal A-246/L	0.8/1.7	0.35	MS (0)
167	5/95	0.16/0.34	Rhodacal A-246/L	0.8/1.7	0.35	MS (0.5)
168	10/90	0.16/0.34	Rhodacal A-246/L	0.8/1.7	0.35	MS (0.5)
169	15/85	0.16/0.34	Rhodacal A-246/L	0.8/1.7	0.35	MS (0.5)

Table 6: Results

Entry	Mn	PDI	Particle size Rh (nm)	Monomer conversion (%)	Solid conversion (%)
2	26597	1.49	36	95	91
3	27015	1.60	44	96	95
4	26348	1.54	34	96	95
5	28577	1.57	48	97	95
6	29205	1.47	36	97	95

Entry	Mn	PDI	Particle size Rh (nm)	Monomer conversion (%)	Solid conversion (%)
7	27259	1.51	29	96	97
8	28441	1.46	34	95	94
9	28637	1.57	32	97	93
10	27020	1.49	30	96	95
11	30412	1.55	27	97	87
12	32075	1.48	32	98	88
13	28149	1.52	27	95	97
14	27700	1.55	43	96	96
15	28794	1.50	31	96	97
16	28720	1.53	34	96	93
17	28131	1.50	29	96	98
18	31388	1.49	31	97	91
19	28072	1.48	32	96	89
20	27628	1.48	33	94	96
21	28600	1.48	29	96	93
22	31603	1.51	26	97	96
23	29065	1.50	27	96	94
24	26831	1.51	28	95	97
25	26317	1.59	27	96	96
26	25300	1.55	56	72	70
27	26700	1.55	50	79	85
28	29000	1.53	28	82	86
29	30600	1.57	36	87	84
30	26400	1.56	48	81	88
31	26300	1.54	23	71	80
32	24600	1.56	27	75	77
33	32100	1.52	28	90	90
34	27600	1.55	39	84	85
35	26100	1.56	38	84	93
36	32200	1.58	25	91	83
37	26900	1.53	38	82	81
38	26700	1.62	53	84	89
39	27100	1.61	29	86	83
40	28600	1.62	30	89	86
41	26400	1.63	33	85	92
42	27600	1.59	29	86	79
43	26600	1.59	27	81	89

Entry	Mn	PDI	Particle size Rh (nm)	Monomer conversion (%)	Solid conversion (%)
44	24700	1.58	39	79	91
45	28400	1.66	35	85	88
46	28900	1.56	35	85	89
47	27700	1.62	41	84	88
48	27700	1.57	33	84	74
49	26300	1.56	39	82	92
50	27400	1.61	73	85	83
51	27900	1.58	32	84	92
52	28800	1.59	25	88	92
53	29600	1.53	34	85	92
54	27800	1.59	25	88	91
55	25200	1.57	23	81	88
56	46700	23.69	36	98	70
57	45100	1.69	50	99	87
58	40400	1.68	42	99	92
59	53000	1.79	36	98	86
60	44200	1.85	42	99	81
61	38600	1.69	34	98	79
62	60400	2.01	64	98	85
63	48000	2.02	73	98	83
64	52200	1.94	61	98	72
65	72100	2.13	43	98	74
66	53600	2.16	69	98	84
67	50200	1.95	65	98	82
68	37500	3.16	38	97	65
69	56500	1.68	62	98	74
70	40100	1.78	66	98	87
71	33300	17.50	57	98	111
72	45900	4.22	63	98	115
73	30600	2.14	54	98	105
74	NA	NA	32	97	97
75	35800	1.81	24	99	75
76	24400	1.70	26	98	92
77	27200	1.61	43	98	93
78	26000	1.62	24	98	91
79	20800	1.61	36	98	94
80	29200	1.70	37	98	96

Entry	Mn	PDI	Particle size Rh (nm)	Monomer conversion (%)	Solid conversion (%)
81	25400	1.60	27	98	95
82	23700	1.63	25	98	97
83	27700	1.67	28	97	94
84	25400	1.66	33	98	98
85	23900	1.61	33	98	99
86	28000	1.78	37	98	97
87	25600	1.64	25	98	95
88	24000	1.64	23	98	97
89	26600	1.69	25	97	97
90	25700	1.62	25	98	97
91	23700	1.70	31	98	99
92	27600	1.86	34	96	86
93	25300	1.64	33	98	98
94	25400	1.62	23	98	97
95	26500	1.78	42	98	98
96	25200	1.62	26	98	101
97	23000	1.66	32	97	100
98	25000	1.76	42	94	102
99	31100	2.25	35	99	59
100	49000	2.67	36	100	68
101	24400	1.77	38	97	106
102	21600	1.67	34	99	98
103	38800	2.61	32	99	77
104	21300	1.91	43	97	99
105	48300	2.49	38	99	70
106	49000	2.87	39	99	66
107	22700	1.61	27	92	104
108	20900	1.82	26	99	99
109	23300	1.90	29	99	90
110	23400	1.81	38	95	99
111	39800	2.64	45	99	68
112	35900	2.59	47	99	69
113	21200	1.66	27	95	97
114	21100	1.67	26	99	93
115	22100	1.91	25	99	85
116	22900	1.66	31	96	83
117	43100	2.11	44	99	65

Entry	Mn	PDI	Particle size Rh (nm)	Monomer conversion (%)	Solid conversion (%)
118	39800	2.32	42	99	69
119	22900	1.62	30	96	96
120	25800	1.91	25	99	81
121	27000	2.08	34	99	70
122	15400	1.49	37	98	65
123	34100	2.01	48	98	80
124	25800	1.74	33	96	96
125	18400	2.93	50	97	97
126	23700	1.80	50	97	101
127	22400	1.68	51	96	101
128	25600	1.62	38	93	98
129	27600	1.75	36	95	97
130	25500	1.61	35	94	96
131	24200	1.90	51	97	101
132	24300	2.10	53	97	101
133	24100	1.66	50	97	97
134	25200	1.68	40	94	95
135	25900	1.80	34	97	98
136	24500	1.61	36	94	99
137	22000	2.36	53	96	97
138	23100	1.97	53	97	99
139	23000	1.86	47	97	105
140	24700	1.66	36	95	99
141	25500	1.83	35	95	95
142	26600	1.82	32	96	95
143	22500	2.06	53	96	101
144	22700	1.96	50	97	101
145	24500	1.75	47	97	99
146	10600	1.70	47	99	84
147	16900	1.76	40	94	102
148	18800	2.14	31	98	92
149	17100	2.09	28	97	97
150	16100	1.92	28	99	101
151	NA	NA	34	96	100
152	15200	1.70	36	91	96
153	18900	2.02	38	98	88
154	14900	1.76	35	95	98

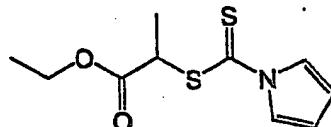
Entry	Mn	PDI	Particle size Rh (nm)	Monomer conversion (%)	Solid conversion (%)
155	14900	1.82	35	97	99
156	15700	1.92	29	97	96
157	14500	1.73	31	95	101
158	14500	1.75	33	93	99
159	18100	2.26	26	97	90
160	15400	1.79	30	96	94
161	13900	1.75	35	95	101
162	15100	2.21	28	97	99
163	13800	1.76	30	96	99
164	12900	1.82	40	90	97
165	14100	1.87	26	95	98
166	14400	2.49	27	97	89
167	13400	2.11	30	97	99
168	12500	1.77	27	95	97
169	12100	1.75	32	95	99

[0142] These examples show that the control agent of this invention provides good latex stability, a quantitative yield of polymer, a controlled molecular weight and low polydispersity, despite a wide variety of polymerization conditions.

5

Comparative Example 19:

[0143] Comparative examples were run in the same manner as example 18 above, but using a different control agent, with the control agent in this example



having the structure: This control agent was prepared in a manner known in the art; see for example, WO 99/31144. Table 7 presents the experimental conditions used in the emulsion polymerizations using this control agent and Table 8 presents the results:

Table 7: Process variables (The numbers are wt% relative to the total monomer)

Entry	Monomer Initial charge/conti nuous addition	Initiator Initial charge/conti nuous addition	Surfactant Type	Surfactant Initial charge/conti nuous addition	NaHCO ₃	Stabilizer type (amount)
170	5/95	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)

Entry	Monomer Initial charge/conti nuous addition	Initiator Initial charge/conti nuous addition	Surfactant Type	Surfactant Initial charge/conti nuous addition	NaHCO ₃	Stabilizer type (amount)
171	10/90	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
172	15/85	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
173	20/80	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
174	25/75	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
175	30/70	0.1/0.4	SDS	0.5/2.0	0.35	MS(0.5)
176	5/95	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
177	10/90	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
178	15/85	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
179	20/80	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
180	25/75	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
181	30/70	0.12/0.38	SDS	0.6/1.9	0.35	MS(0.5)
182	5/95	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
183	10/90	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
184	15/85	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
185	20/80	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
186	25/75	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
187	30/70	0.14/0.36	SDS	0.7/1.8	0.35	MS(0.5)
188	5/95	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
189	10/90	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
190	15/85	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
191	20/80	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
192	25/75	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)
193	30/70	0.16/0.34	SDS	0.8/1.7	0.35	MS(0.5)

Table 8: Results for Comparative Example

Entry	Mn	PDI	Particle size Rh (nm)	Monomer conversion (%)	Solid conversion (%)
170	162626	16.04	42	99	99
171	222086	25.53	44	98	103
172	168762	50	36	99	101
173	204592	33.79	38	99	102
174	190414	35.18	39	99	105
175	114566	7.33	43	99	102
176	168770	31.83	46	98	100
177	180454	33.38	39	98	101

Entry	Mn	PDI	Particle size Rh (nm)	Monomer conversion (%)	Solid conversion (%)
178	212703	27.76	44	98	101
179	166667	21.95	42	98	101
180	199547	42.46	35	99	101
181	192968	31.62	36	99	102
182	207935	29.51	41	98	100
183	160429	39.46	35	99	102
184	257670	28.52	38	98	101
185	70404	7.37	39	99	101
186	169302	40.86	32	99	102
187	218549	30.91	36	99	102
188	152887	29.89	41	98	102
189	155982	36.14	36	98	99
190	226514	34.05	36	98	101
191	162853	36.14	32	99	101
192	187029	29.57	32	98	101
193	133599	22.45	33	99	101

[0144] These results show that the control agent in this comparative example does not provide control over the molecular weight and leads to broad molecular weight distributions with a polydispersity index greater than 10 under emulsion conditions.

5

EXAMPLE 20:

10

[0145] Diblock copolymerization of *n*-butyl acrylate/styrene in emulsion can be accomplished using the control agent C-1, whose synthesis is described above. The polymerization is carried out in one-pot procedure, where the second monomer and additional initiator are introduced subsequently after polymerization of first monomer is complete. The first block of poly *n*-butyl acrylate is prepared using the conditions described in example 18, above. This results in poly *n*-butyl acrylate emulsion at 80 °C to which styrene in amount of 813mg and 1.5mL of sodium persulfate aqueous solution in 0.33 wt% concentration are semi-continuously added over the course of 6 and 7 hours, respectively. The reaction mixture is then stirred for an additional 2 hours after

15

the last addition is finished. A stable emulsion is formed and its detail characterization is reported in Table 9.

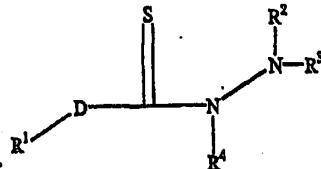
Table 9: Result of poly(*n*-butyl acrylate)-block-polystyrene

Example	Mn	PDI	Particle size Rh (nm)	Monomer conversion BA/Styrene (%)	Solid conversion (%)
194	47059	1.80	65	99/95	98

[0146] It is to be understood that the above description is intended to be
5 illustrative and not restrictive. Many embodiments will be apparent to those of
skill in the art upon reading the above description. The scope of the invention
should, therefore, be determined not with reference to the above description, but
should instead be determined with reference to the appended claims, along with
the full scope of equivalents to which such claims are entitled. The disclosures of
10 all articles and references, including patent applications and publications, are
incorporated herein by reference for all purposes.

What is claimed is:

1 1. A method of free radical polymerization comprising (1) forming a mixture of one
2 or more monomers, at least one free radical source and a control agent and (2) subjecting
3 said mixture to polymerization conditions, wherein said control agent is characterized by



4 the general formula:

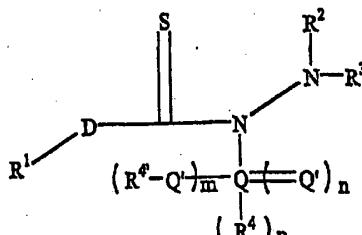
5 wherein R¹ is any group that can be expelled as its free radical form in an
6 addition-fragmentation reaction;

7 R² and R³ are each independently selected from the group consisting of hydrogen,
8 hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and
9 substituted heteroatom-containing hydrocarbyl, and combinations thereof, and optionally
10 R² and R³ together to form a double bond optionally substituted alkenyl moiety;

11 R^4 is selected from the group consisting of hydrogen, hydrocarbyl, substituted
12 hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing
13 hydrocarbyl, and combinations thereof; and optionally, R^4 combines with R^2 and/or R^3 to
14 form a ring structure, with said ring having from 3 to 50 non-hydrogen atoms; and

15 D is either sulfur, selenium or tellurium.

2 The method of claim 1 wherein said control agent is characterized by the general

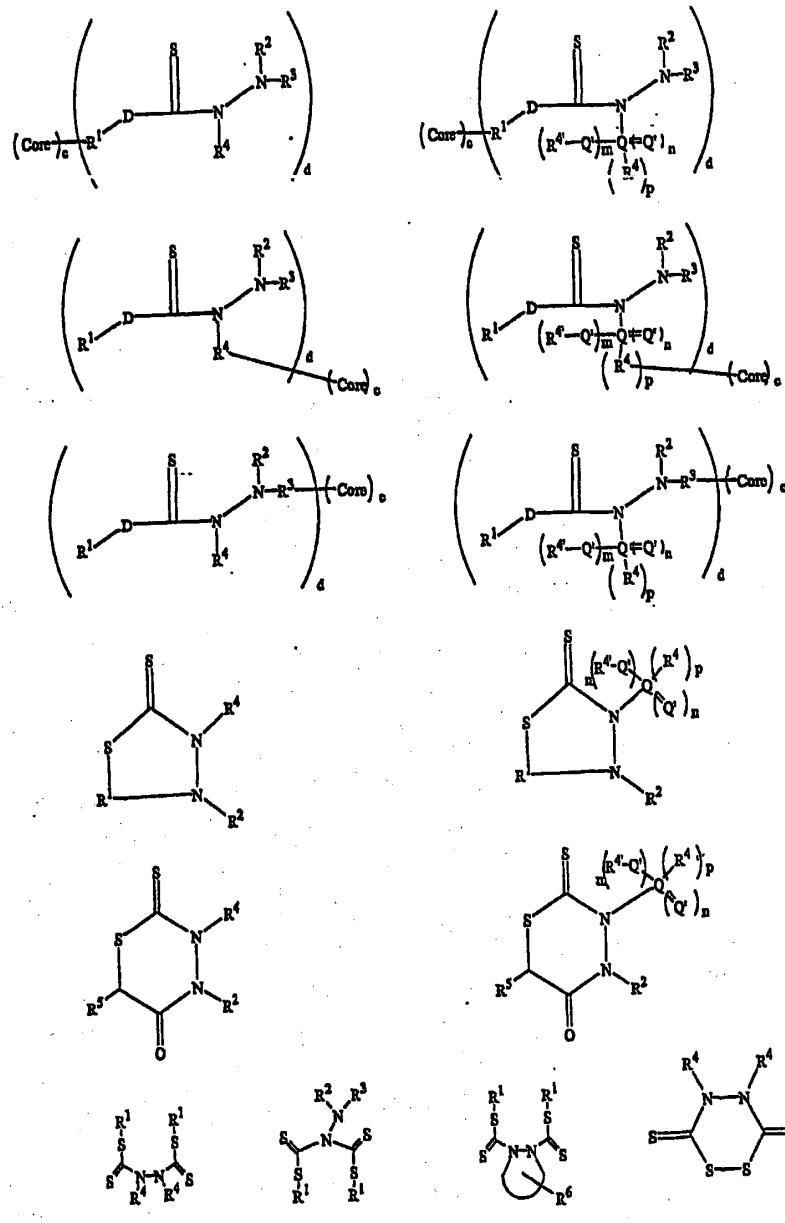


2 formula: $(R^4)_p$ wherein Q is selected from the group
3 consisting of carbon, sulfur and phosphorus; Q' is selected from the group consisting of
4 oxygen and sulfur; R⁴ is selected from the same group as R⁴; and each of n, m and p is 0,
5 1 or 2 to satisfy the valency of Q.

1 3. The method of either of claims 1 or 2, wherein an initiator is the source of free
2 radicals.

- 1 4. The method of claim 3 wherein D is sulfur, Q is carbon, Q' is oxygen and n is 1.
- 1 5. The method of claim 4, wherein R⁴ is selected from the group consisting of
2 optionally substituted alkyl and optionally substituted aryl.
- 1 6. The method of any of the proceeding claims, wherein R¹ is selected from the
2 group consisting of optionally substituted alkyl, optionally substituted aryl, optionally
3 substituted alkenyl, optionally substituted alkoxy, optionally substituted heterocycl,
4 optionally substituted alkylthio, optionally substituted amino and optionally substituted
5 polymer chains.
- 1 7. The method of any of the proceeding claims, wherein R¹ is selected from the
2 group consisting of -CH₂Ph, -CH(CH₃)CO₂CH₂CH₃, -CH(CO₂CH₂CH₃)₂,
3 -C(CH₃)₂CN, -CH(Ph)CN and -C(CH₃)₂Ph.
- 1 8. The method of any of the proceeding claims, wherein R² and R³ are each
2 independently selected from the group consisting of hydrogen, optionally substituted
3 alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted
4 acyl, optionally substituted, aroyl, optionally substituted alkoxy, optionally substituted
5 heteroaryl, optionally substituted heterocycl, optionally substituted alkylsulfonyl,
6 optionally substituted alkylsulfinyl, optionally substituted alkylphosphonyl, optionally
7 substituted arylsulfinyl, and optionally substituted arylphosphonyl.
- 1 9. The method of any of the proceeding claims, wherein two or more monomers are
2 added to said polymerization mixture and said two or more monomers are added
3 sequentially or simultaneously.
- 1 10. The method of either of claims 1, 2 or 3, wherein said polymerization conditions
2 comprise living kinetics.
- 1 11. A polymer formed by the method of any of any of the proceeding claims.
- 1 12. A method of method of free radical polymerization comprising (1) forming a
2 mixture of one or more monomers, at least one free radical source and a multi-functional
3 control agent and (2) subjecting said mixture to polymerization conditions, wherein said

4 multi-functional control agent is selected from any of the following formulas:



6 wherein R¹ is any group that can be expelled as its free radical form in an
 7 addition-fragmentation reaction;
 8 R² and R³ are each independently selected from the group consisting of hydrogen,
 9 hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and
 10 substituted heteroatom-containing hydrocarbyl, and combinations thereof; and optionally
 11 R² and R³ together to form a double bond optionally substituted alkenyl moiety;
 12 R⁴ and R^{4'} are each independently selected from the group consisting of hydrogen,
 13 hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and

14 substituted heteroatom-containing hydrocarbyl, and combinations thereof; and
 15 optionally, R^4 combines with R^2 and/or R^3 to form a ring structure, with said ring having
 16 from 3 to 50 non-hydrogen atoms;

17 D is either sulfur, selenium or tellurium;

18 Q is selected from the group consisting of carbon, sulfur and phosphorus; Q' is
 19 selected from the group consisting of oxygen and sulfur; and each of n , m and p is 0, 1 or
 20 2 to satisfy the valency of Q ;

21 Core is a core molecule, and c is 1 or more and d is 2 or more;

22 R^5 is selected from the group consisting of hydrogen, hydrocarbyl, substituted
 23 hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing
 24 hydrocarbyl, and combinations thereof;



25 R^6 refers to a ring structure having between 3 and 20 non-hydrogen
 26 atoms in the ring, including single ring or multiple rings that are fused together, linked
 27 covalently, or linked to a common group; and

28 R^6 is a substituent on any member of the ring other than the two shown nitrogen
 29 atoms.

1 13. The method of claim 12, wherein an initiator is the source of free radicals.

1 14. The method of claim 13, wherein R^1 is selected from the group consisting of
 2 optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl,
 3 optionally substituted alkoxy, optionally substituted heterocycl, optionally substituted
 4 alkylthio, optionally substituted amino and optionally substituted polymer chains.

1 15. The method of claim 14, wherein R^1 is selected from the group consisting of—
 2 CH_2Ph , $-CH(CH_3)CO_2CH_2CH_3$, $-CH(CO_2CH_2CH_3)_2$, $-C(CH_3)_2CN$, $-CH(Ph)CN$ and $-$
 3 $C(CH_3)_2Ph$.

1 16. The method of any of the proceeding claims, wherein R^2 and R^3 are each
 2 independently selected from the group consisting of hydrogen, optionally substituted
 3 alkyl, optionally substituted aryl, optionally substituted alkenyl, optionally substituted
 4 acyl, optionally substituted, aroyl, optionally substituted alkoxy, optionally substituted

5 heteroaryl, optionally substituted heterocycl, optionally substituted alkylsulfonyl,
 6 optionally substituted alkylsulfinyl, optionally substituted alkylphosphonyl, optionally
 7 substituted arylsulfinyl, and optionally substituted arylphosphonyl.

1 17. The method of any of the proceeding claims, wherein R⁴ is selected from the
 2 group consisting of hydrogen, optionally substituted alkyl, optionally substituted aryl,
 3 amino, thio, optionally substituted aryloxy and optionally substituted alkoxy.

1 18. The method of any of the proceeding claims, wherein said polymerization
 2 conditions comprise a temperature in the range of from about 20°C to about 110°C.

1 19. The method of any of the proceeding claims, wherein two or more monomers are
 2 added to said polymerization mixture and said two or more monomers are added
 3 sequentially or simultaneously.

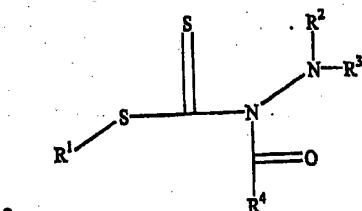
1 20. The method of any of the proceeding claims, wherein said polymerization
 2 conditions comprise living kinetics.

1 21. A polymer formed by the method of any of the proceeding claims.

1 22. The polymer of claim 21, wherein said copolymer is a block copolymer.

1 23. The polymer of claim 21, wherein said polymer is a star or hyperbranched
 2 polymer.

1 24. A compound characterized by the formula:



2 3 wherein R¹ is selected from the group consisting of hydrocarbyl, substituted
 4 hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing
 5 hydrocarbyl, and combinations thereof, with the proviso that R¹ is not methyl;

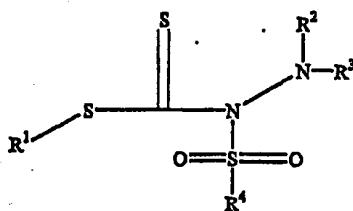
6 R² and R³ are each independently selected from the group consisting of hydrogen,
 7 hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and
 8 substituted heteroatom-containing hydrocarbyl, and combinations thereof, and

9 R⁴ is selected from the group consisting of hydrogen, hydrocarbyl, substituted
 10 hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing
 11 hydrocarbyl, and combinations thereof; and optionally, R⁴ combines with R² and/or R³ to
 12 form a ring structure, with said ring having from 3 to 50 non-hydrogen atoms.

1 25. The compound of claim 24, wherein R¹ is selected from the group consisting
 2 of -CH₂Ph, -CH(CH₃)CO₂CH₂CH₃, -CH(CO₂CH₂CH₃)₂, -C(CH₃)₂CN and -C(CH₃)₂Ph.

1 26. The compound of claim 24, wherein R² and R³ are each independently selected
 2 from the group consisting of hydrogen, optionally substituted alkyl, optionally
 3 substituted aryl, optionally substituted alkenyl, optionally substituted acyl, optionally
 4 substituted, aroyl, optionally substituted alkoxy, optionally substituted heteroaryl,
 5 optionally substituted heterocyclyl, optionally substituted alkylsulfonyl, optionally
 6 substituted alkylsulfinyl, optionally substituted alkylphosphonyl, optionally substituted
 7 arylsulfinyl, and optionally substituted arylphosphonyl.

1 27. A compound characterized by the formula:



3 wherein R¹ is selected from the group consisting of hydrocarbyl, substituted
 4 hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing
 5 hydrocarbyl, and combinations thereof;

6 R² and R³ are each independently selected from the group consisting of hydrogen,
 7 hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and
 8 substituted heteroatom-containing hydrocarbyl, and combinations thereof, and

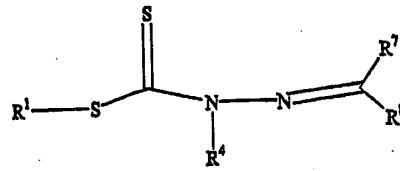
9 R⁴ is selected from the group consisting of hydrogen, hydrocarbyl, substituted
 10 hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-containing
 11 hydrocarbyl, and combinations thereof; and optionally, R⁴ combines with R² and/or R³ to
 12 form a ring structure, with said ring having from 3 to 50 non-hydrogen atoms.

1 28. The compound of claim 27, wherein R¹ is selected from the group consisting
 2 of -CH₂Ph, -CH(CH₃)CO₂CH₂CH₃, -CH(CO₂CH₂CH₃)₂, -C(CH₃)₂CN and

3 -C(CH₃)₂Ph.

1 29. The compound of claim 28, wherein R² and R³ are each independently selected
 2 from the group consisting of hydrogen, optionally substituted alkyl, optionally
 3 substituted aryl, optionally substituted alkenyl, optionally substituted acyl, optionally
 4 substituted, aroyl, optionally substituted alkoxy, optionally substituted heteroaryl,
 5 optionally substituted heterocycl, optionally substituted alkylsulfonyl, optionally
 6 substituted alkylsulfinyl, optionally substituted alkylphosphonyl, optionally substituted
 7 arylsulfinyl, and optionally substituted arylphosphonyl.

1 30. A method of free radical polymerization comprising (1) forming a mixture of one
 2 or more monomers, water, optionally surfactant, at least one free radical source and a
 3 control agent and (2) subjecting said mixture to polymerization conditions, wherein said
 4 control agent is characterized by the general formula:



5 wherein R¹ is generally any group that is sufficiently labile to be expelled as its
 6 free radical form; R⁴ is selected from the group consisting of hydrogen, hydrocarbyl,
 7 substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-
 8 containing hydrocarbyl, and combinations thereof; and
 9

10 R⁷ and R⁸ are independently selected from the group consisting of hydrogen,
 11 hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and
 12 substituted heteroatom-containing hydrocarbyl, and combinations thereof.

1 31. The method of claim 30, wherein R⁴ is selected from the group consisting of
 2 optionally substituted alkyl and optionally substituted aryl.

1 32. The method of claim 30, wherein R¹ is selected from the group consisting of -
 2 CH₂Ph, -CH(CH₃)CO₂CH₂CH₃, -CH(CO₂CH₂CH₃)₂, -C(CH₃)₂CN, -CH(Ph)CN and -
 3 C(CH₃)₂Ph.

1 33. The method of claim 30, wherein R⁷ and R⁸ are each independently selected from
 2 the group consisting of hydrogen, optionally substituted alkyl, optionally substituted aryl,

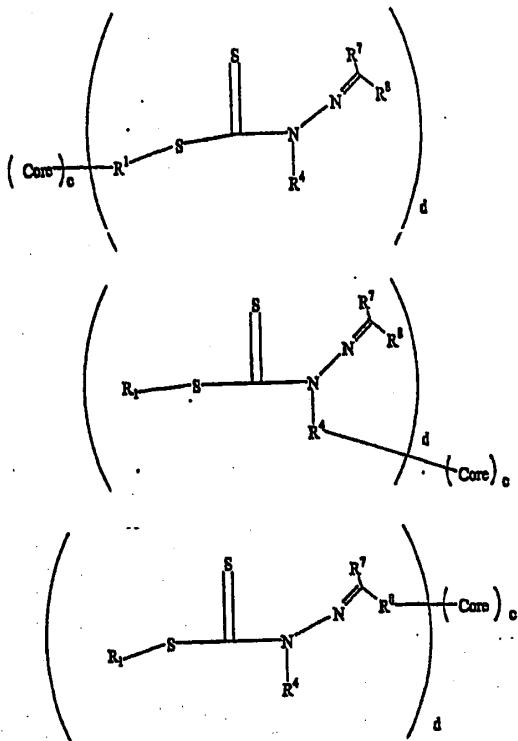
3 optionally substituted alkenyl, optionally substituted acyl, optionally substituted, aroyl,
4 optionally substituted alkoxy, optionally substituted heteroaryl, optionally substituted
5 heterocycll, optionally substituted alkylsulfonyl, optionally substituted alkylsulfinyl,
6 optionally substituted alkylphosphonyl, optionally substituted arylsulfinyl, and optionally
7 substituted arylphosphonyl.

1 34. The method of claim 30, wherein two or more monomers are added to said
2 polymerization mixture and said two or more monomers are added sequentially or
3 simultaneously.

1 35. The method of claim 30, wherein said polymerization conditions comprise a
2 continuous or semi-continuous addition of reagent to said mixture, wherein said addition
3 of reagent comprises addition of said one or more monomers, surfactant, initiator and
4 combinations thereof.

1 36. A polymer formed by the method of claim 30.

1 37. A method of method of heterogeneous free radical polymerization comprising (1)
2 forming a heterogeneous mixture of one or more monomers, at least one free radical
3 source, water, optionally surfactant and a multi-functional control agent and (2)
4 subjecting said heterogeneous mixture to polymerization conditions, wherein said multi-
5 functional control agent is selected from any of the following formulas:



6 wherein Core is a multi-functional core molecule, and c is 1 or more and d is 2 or
7
8 more;

9 wherein R^1 is generally any group that is sufficiently labile to be expelled as its
10 free radical form; R^4 is selected from the group consisting of hydrogen, hydrocarbyl,
11 substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and substituted heteroatom-
12 containing hydrocarbyl, and combinations thereof; and

13 R⁷ and R⁸ are independently selected from the group consisting of hydrogen,
14 hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and
15 substituted heteroatom-containing hydrocarbyl, and combinations thereof R⁶ is a
16 substituent on any member of the ring other than the two shown nitrogen atoms.

1 38. The method of claim 37, wherein R^1 is selected from the group consisting of
2 optionally substituted alkyl, optionally substituted aryl, optionally substituted alkenyl,
3 optionally substituted alkoxy, optionally substituted heterocycl, optionally substituted
4 alkylthio, optionally substituted amino and optionally substituted polymer chains.

1 39. The method of claim 37, wherein R⁷ and R⁸ are each independently selected from
2 the group consisting of hydrogen, optionally substituted alkyl, optionally substituted aryl,
3 optionally substituted alkenyl, optionally substituted acyl, optionally substituted, aroyl,

4 optionally substituted alkoxy, optionally substituted heteroaryl, optionally substituted
 5 heterocycll, optionally substituted alkylsulfonyl, optionally substituted alkylsulfinyl,
 6 optionally substituted alkylphosphonyl, optionally substituted arylsulfinyl, and optionally
 7 substituted arylphosphonyl.

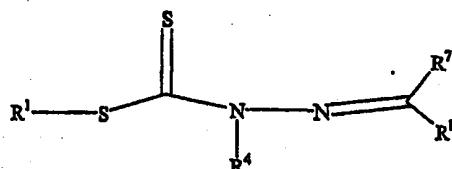
1 40. The method of claim 37, wherein two or more monomers are added to said
 2 heterogeneous polymerization mixture and said two or more monomers are added
 3 sequentially or simultaneously.

1 41. A polymer formed by the method of claim 37.

1 42. The polymer of claim 41, wherein said copolymer is a block copolymer.

1 43. The polymer of claim 41, wherein said polymer is a star or hyperbranched
 2 polymer.

1 44. A compound characterized by the general formula:



2 wherein R¹ is generally any group that is
 3 sufficiently labile to be expelled as its free radical form; R⁴ is selected from the group
 4 consisting of hydrogen, hydrocarbyl, substituted hydrocarbyl, heteroatom-containing
 5 hydrocarbyl, and substituted heteroatom-containing hydrocarbyl, and combinations
 6 thereof; and
 7 R⁷ and R⁸ are independently selected from the group consisting of hydrogen,
 8 hydrocarbyl, substituted hydrocarbyl, heteroatom-containing hydrocarbyl, and
 9 substituted heteroatom-containing hydrocarbyl, and combinations thereof.

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
4 April 2002 (04.04.2002)

PCT

(10) International Publication Number
WO 02/26836 A3

(51) International Patent Classification⁷: C08F 2/38. 293/00, C07C 337/08

C08F 2/38.

(81) Designated States (national): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, UZ, VN, YU, ZA, ZW.

(21) International Application Number: PCT/US01/30066

(22) International Filing Date:
26 September 2001 (26.09.2001)

(25) Filing Language:

English

(26) Publication Language:

English

(30) Priority Data:

09/676,267 28 September 2000 (28.09.2000) US
09/963,172 25 September 2001 (25.09.2001) US

(84) Designated States (regional): ARIPO patent (GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

(71) Applicant: SYMYX TECHNOLOGIES, INC. [—/US];
3100 Central Expressway, Santa Clara, CA 95051 (US).

Published:

- with international search report
- before the expiration of the time limit for amending the claims and to be republished in the event of receipt of amendments

(72) Inventors: CHARMOT, Dominique; 1238 Bracebridge Court, Campbell, CA 95008 (US). CHANG, Han, Ting; 220 Garnet Drive, Livermore, CA 94550 (US). LI, Yunxiao; 737E, El Camino Real, Sunnyvale, CA 94087 (US). HUEFNER, Peter; 634 Celebration Court, San Jose, CA 95134 (US).

(88) Date of publication of the international search report:
27 June 2002

(74) Agent: KRASNOW, Ronald, A.; Symyx Technologies, Inc., 3100 Central Expressway, Santa Clara, CA 95051 (US).

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

WO 02/26836 A3

(54) Title: CONTROL AGENTS FOR LIVING-TYPE FREE RADICAL POLYMERIZATION, METHODS OF POLYMERIZING, EMULSIONS AND POLYMERS WITH SAME

(57) Abstract: Control agents that have a nitrogen-nitrogen bond covalently bonded to a thiocarbonyl moiety are provided for living-type free radical polymerization of a wide variety of monomers. These control agents provide superior properties for control of the polymerization and/or the properties of the polymers obtained and/or the monomers that may be polymerized. In some embodiments, a bulky group is pendant off the activated thiocarbonyl portion of the control agents. Multifunctional control agents provide the opportunity for a variety of structurally unique polymers, including block copolymers, stars and hyper-branched polymers.

INTERNATIONAL SEARCH REPORT

International Application No
PCT/US 01/30066A. CLASSIFICATION OF SUBJECT MATTER
IPC 7 C08F2/38 C08F293/00 C07C337/08

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 7 C08F C07C

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the International search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	FR 2 764 892 A (RHODIA CHIMIE) 24 December 1998 (1998-12-24) cited in the application	
A	WO 99 31144 A (E.I. DU PONT DE NEMOURS) 24 December 1999 (1999-12-24) cited in the application	

 Further documents are listed in the continuation of box C. Patent family members are listed in annex.

* Special categories of cited documents:

- *A* document defining the general state of the art which is not considered to be of particular relevance
- *E* earlier document but published on or after the International filing date
- *L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- *O* document referring to an oral disclosure, use, exhibition or other means
- *P* document published prior to the international filing date but later than the priority date claimed

T later document published after the International filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

X document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

Y document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

& document member of the same patent family

Date of the actual completion of the International search

Date of mailing of the International search report

16 April 2002

24/04/2002

Name and mailing address of the ISA
European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl.
Fax: (+31-70) 340-3016

Authorized officer

Cauwenberg, C

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/US 01/30066

Patent document cited in search report	Publication date	Patent family member(s)		Publication date
FR 2764892	A 24-12-1998	FR	2764892 A1	24-12-1998
		AU	740771 B2	15-11-2001
		AU	8342598 A	04-01-1999
		BR	9810289 A	19-09-2000
		CN	1268958 T	04-10-2000
		EP	0991683 A1	12-04-2000
		WO	9858974 A1	30-12-1998
		HU	0002090 A2	28-10-2000
		NO	996389 A	23-02-2000
		PL	337608 A1	28-08-2000
		SK	174199 A3	12-06-2000
		US	6153705 A	28-11-2000
		ZA	9805450 A	06-01-1999
WO 9931144	A 24-06-1999	AU	1911399 A	05-07-1999
		BR	9815179 A	10-10-2000
		CA	2309279 A1	24-06-1999
		EP	1054906 A1	29-11-2000
		WO	9931144 A1	24-06-1999

THIS PAGE BLANK (USPTO)